

(19) World Intellectual Property Organization
International Bureau(43) International Publication Date
19 December 2002 (19.12.2002)

PCT

(10) International Publication Number
WO 02/101120 A2(51) International Patent Classification⁷: **C30B**

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(21) International Application Number: PCT/IB02/04185

(22) International Filing Date: 17 May 2002 (17.05.2002)

(25) Filing Language: English

(26) Publication Language: English

(30) Priority Data:
P-347918 6 June 2001 (06.06.2001) PL
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(81) Designated States (national): AE, AG, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, BZ, CA, CH, CN, CO, CR, CU, CZ, DE, DK, DM, DZ, EC, EE, ES, FI, GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MA, MD, MG, MK, MN, MW, MX, MZ, NO, NZ, OM, PH, PL, PT, RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TN, TR, TT, TZ, UA, UG, US, UZ, VN, YU, ZA, ZM, ZW.

(84) Designated States (regional): ARIPO patent (GH, GM, KE, LS, MW, MZ, SD, SL, SZ, TZ, UG, ZM, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE, TR), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, GQ, GW, ML, MR, NE, SN, TD, TG).

Published:

— without international search report and to be republished upon receipt of that report

For two-letter codes and other abbreviations, refer to the "Guidance Notes on Codes and Abbreviations" appearing at the beginning of each regular issue of the PCT Gazette.

(54) Title: PROCESS AND APPARATUS FOR OBTAINING BULK MONOCRYSTALLINE GALLIUM-CONTAINING NITRIDE

(57) Abstract: The present invention refers to an ammonobasic method for preparing a gallium-containing nitride crystal, in which gallium-containing feedstock is crystallized on at least one crystallization seed in the presence of an alkali metal-containing component in a supercritical nitrogen-containing solvent. The method can provide monocrySTALLINE gallium-containing nitride crystals having a very high quality.

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WO 02/101120 A2

PROCESS AND APPARATUS FOR OBTAINING BULK MONOCRYSTALLINE GALLIUM-CONTAINING NITRIDE

The present invention refers to processes for obtaining a gallium-containing nitride
5 crystal by an ammonobasic method as well as the gallium-containing nitride crystal itself.
Furthermore, an apparatus for conducting the various methods is disclosed.

Optoelectronic devices based on nitrides are usually manufactured on sapphire or
silicon carbide substrates that differ from the deposited nitride layers (so-called
heteroepitaxy). In the most often used Metallo-Organic Chemical Vapor Deposition
10 (MOCVD) method, the deposition of GaN is performed from ammonia and organometallic
compounds in the gas phase and the growth rates achieved make it impossible to provide a
bulk layer. The application of a buffer layer reduces the dislocation density, but not more
than to approx. $10^8/\text{cm}^2$. Another method has also been proposed for obtaining bulk
monocrystalline gallium nitride. This method consists of an epitaxial deposition
15 employing halides in a vapor phase and is called Halide Vapor Phase Epitaxy (HVPE)
["Optical patterning of GaN films" M.K. Kelly, O. Ambacher, Appl. Phys. Lett. 69 (12),
(1996) and "Fabrication of thin-film InGaN light-emitting diode membranes" W.S. Wong,
T. Sands, Appl. Phys. Lett. 75 (10) (1999)]. This method allows for the preparation of
GaN substrates having a 2-inch (5 cm) diameter.

20 However, their quality is not sufficient for laser diodes, because the dislocation
density continues to be approx. 10^7 to approx. $10^9/\text{cm}^2$. Recently, the method of Epitaxial
Lateral OverGrowth (ELOG) has been used for reducing the dislocation density. In this
method the GaN layer is first grown on a sapphire substrate and then a layer with SiO_2 is
deposited on it in the form of strips or a lattice. On the thus prepared substrate, in turn, the
25 lateral growth of GaN may be carried out leading to a dislocation density of approx.
 $10^7/\text{cm}^2$.

The growth of bulk crystals of gallium nitride and other metals of group XIII (IUPAC, 1989) is extremely difficult. Standard methods of crystallization from melt and sublimation methods are not applicable because of the decomposition of the nitrides into metals and N_2 . In the High Nitrogen Pressure (HNP) method ["Prospects for high-pressure crystal growth of III-V nitrides" S. Porowski *et al.*, Inst. Phys. Conf. Series, 137, 369 (1998)] this decomposition is inhibited by the use of nitrogen under the high pressure. The growth of crystals is carried out in molten gallium, i.e. in the liquid phase, resulting in the production of GaN platelets about 10 mm in size. Sufficient solubility of nitrogen in gallium requires temperatures of about 1500 °C and nitrogen pressures in the order of 15 kbar.

The use of supercritical ammonia has been proposed to lower the temperature and decrease the pressure during the growth process of nitrides. Peters has described the ammonothermal synthesis of aluminium nitride [J. Cryst. Growth 104, 411-418 (1990)]. R. Dwiliński *et al.* have shown, in particular, that it is possible to obtain a fine-crystalline gallium nitride by a synthesis from gallium and ammonia, provided that the latter contains alkali metal amides (KNH_2 or $LiNH_2$). The processes were conducted at temperatures of up to 550 °C and under a pressure of 5 kbar, yielding crystals about 5 μm in size ["AMMONO method of BN, AlN, and GaN synthesis and crystal growth", Proc. EGW-3, Warsaw, June 22-24, 1998, MRS Internet Journal of Nitride Semiconductor Research, <http://nsr.mij.mrs.org/3/25>]. Another supercritical ammonia method, where a fine-crystalline GaN is used as a feedstock together with a mineralizer consisting of an amide (KNH_2) and a halide (KI) also provided for recrystallization of gallium nitride ["Crystal growth of gallium nitride in supercritical ammonia" J.W. Kolis *et al.*, J. Cryst. Growth 222, 431-434 (2001)]. The recrystallization process conducted at 400 °C and 3.4 kbar resulted in GaN crystals about 0.5 mm in size. A similar method has also been described in Mat. Res. Soc. Symp. Proc. Vol. 495, 367-372 (1998) by J.W. Kolis *et al.* However, using these supercritical ammonia processes, no production of bulk monocrystalline was achieved because no chemical transport processes were observed in the supercritical solution, in particular no growth on seeds was conducted.

Therefore, there was a need for an improved method of preparing a gallium-containing nitride crystal.

The lifetime of optical semiconductor devices depends primarily on the crystalline quality of the optically active layers, and especially on the surface dislocation density. In case of GaN based laser diodes, it is beneficial to lower the dislocation density in the GaN substrate layer to less than $10^6/\text{cm}^2$, and this has been extremely difficult to achieve using the methods known so far. Therefore, there was a need for gallium-containing nitride crystals having a quality suitable for use as substrates for optoelectronics.

The subject matter of the present invention is recited in the appended claims. In particular, in one embodiment the present invention refers to a process for obtaining a gallium-containing nitride crystal, comprising the steps of:

- (i) providing a gallium-containing feedstock, an alkali metal-containing component, at least one crystallization seed and a nitrogen-containing solvent in at least one container;
- 15 (ii) bringing the nitrogen-containing solvent into a supercritical state;
- (iii) at least partially dissolving the gallium-containing feedstock at a first temperature and at a first pressure; and
- (iv) crystallizing gallium-containing nitride on the crystallization seed at a second temperature and at a second pressure while the nitrogen-containing solvent is in the supercritical state;
- 20

wherein at least one of the following criteria is fulfilled:

- (a) the second temperature is higher than the first temperature; and
- (b) the second pressure is lower than the first pressure.

In a second embodiment a process for preparing a gallium-containing nitride crystal is described which comprises the steps of:

- (i) providing a gallium-containing feedstock comprising at least two different components, an alkali metal-containing component, at least one crystallization seed and a nitrogen-containing solvent in a container having a dissolution zone and a crystallization zone, whereby the gallium-containing feedstock is provided in the

- dissolution zone and the at least one crystallization seed is provided in the crystallization zone;
- (ii) subsequently bringing the nitrogen-containing solvent into a supercritical state;
 - (iii) subsequently partially dissolving the gallium-containing feedstock at a dissolution temperature and at a dissolution pressure in the dissolution zone, whereby a first component of the gallium-containing feedstock is substantially completely dissolved and a second component of the gallium-containing feedstock as well as the crystallization seed remain substantially undissolved so that an undersaturated or saturated solution with respect to gallium-containing nitride is obtained;
 - (iv) subsequently setting the conditions in the crystallization zone at a second temperature and at a second pressure so that over-saturation with respect to gallium-containing nitride is obtained and crystallization of gallium-containing nitride occurs on the at least one crystallization seed and simultaneously setting the conditions in the dissolution zone at a first temperature and at a first pressure so that the second component of the gallium-containing feedstock is dissolved;
- wherein the second temperature is higher than the first temperature.

A gallium-containing nitride crystal obtainable by one of these processes is also described. Further subject matter of the invention are a gallium-containing nitride crystal having a surface area of more than 2 cm^2 and having a dislocation density of less than $10^6 / \text{cm}^2$ and a gallium-containing nitride crystal having a thickness of at least $200 \text{ }\mu\text{m}$ and a full width at half maximum (FWHM) of X-ray rocking curve from (0002) plane of 50 arcsec or less.

The invention also provides an apparatus for obtaining a gallium-containing nitride crystal comprising an autoclave 1 having an internal space and comprising at least one device 4, 5 for heating the autoclave to at least two zones having different temperatures, wherein the autoclave comprises a device which separates the internal space into a dissolution zone 13 and a crystallization zone 14.

In a yet another embodiment, a process for preparing a bulk monocrystalline gallium-containing nitride in an autoclave is disclosed, which comprises the steps of providing a supercritical ammonia solution containing gallium-containing nitride with ions of alkali metals, and recrystallizing said gallium-containing nitride selectively on a crystallization seed from said supercritical ammonia solution by means of the negative temperature coefficient of solubility and/or by means of the positive pressure coefficient of solubility.

A process for controlling recrystallization of a gallium-containing nitride in a supercritical ammonia solution which comprises steps of providing a supercritical ammonia solution containing a gallium-containing nitride as a gallium complex with ions of alkali metal and NH_3 solvent in an autoclave and decreasing the solubility of said gallium-containing nitride in the supercritical ammonia solution at a temperature less than that of dissolving gallium-containing nitride crystal and/or at a pressure higher than that of dissolving gallium-containing nitride crystal is also disclosed.

Fig. 1 shows the dependency of the solubility of gallium-containing nitride in supercritical ammonia that contains potassium amide (with $\text{KNH}_2:\text{NH}_3=0.07$) on pressure at $T=400^\circ\text{C}$ and $T=500^\circ\text{C}$.

Fig. 2 shows the diagram of time variations of temperature in an autoclave at constant pressure for Example 1.

Fig. 3 shows the diagram of time variations of pressure in an autoclave at constant temperature for Example 2.

Fig. 4 shows the diagram of time variations of temperature in an autoclave at constant volume for Example 3.

Fig. 5 shows the diagram of time variations of temperature in an autoclave for Example 4.

Fig. 6 shows the diagram of time variations of temperature in an autoclave for Example 5.

Fig. 7 shows the diagram of time variations of temperature in an autoclave for Example 6.

Fig. 8 shows the diagram of time variations of temperature in an autoclave for Example 7.

5 Fig. 9 shows a schematic axial cross section of an autoclave as employed in many of the examples, mounted in the furnace.

Fig. 10 is a schematic perspective drawing of an apparatus according to the present invention.

10 Fig. 11 shows the diagram of time variations of temperature in an autoclave at constant volume for Example 8.

Fig. 12 shows the diagram of time variations of temperature in an autoclave at constant volume for Example 9.

Fig. 13 shows the diagram of time variations of temperature in an autoclave at constant volume for Example 10.

15 Fig. 14 shows the diagram of time variations of temperature in an autoclave at constant volume for Examples 11 and 12.

Fig. 15 illustrates the postulated theory of the invention.

In the present invention the following definitions apply:

20 **Gallium-containing nitride** means a nitride of gallium and optionally other element(s) of group XIII (according to IUPAC, 1989). It includes, but is not restricted to, the binary compound GaN, ternary compounds such as AlGa₂N, InGa₂N and also AlInGa₂N (The mentioned formulas are only intended to give the components of the nitrides. It is not intended to indicate their relative amounts).

Bulk monocrystalline gallium-containing nitride means a monocrystalline substrate made of gallium-containing nitride from which e.g. optoelectronic devices such as LED or LD can be formed by epitaxial methods such as MOCVD and HVPE.

Supercritical solvent means a fluid in a supercritical state. It can also contain other components in addition to the solvent itself as long as these components do not substantially influence or disturb the function of the supercritical solvent. In particular, the solvent can contain ions of alkali metals.

Supercritical solution is used when referring to the supercritical solvent when it contains gallium in a soluble form originating from the dissolution of gallium-containing feedstock.

Dissolution of gallium-containing feedstock means a process (either reversible or irreversible) in which said feedstock is taken up into the supercritical solvent as gallium in a soluble form, possibly as gallium complex compounds.

Gallium complex compounds are complex compounds, in which a gallium atom is a coordination center surrounded by ligands, such as NH_3 molecules or its derivatives, like NH_2^- , NH^{2-} , etc.

Negative temperature coefficient of solubility means that the solubility of a respective compound is a monotonically decreasing function of temperature if all other parameters are kept constant. Similarly, **positive pressure coefficient of solubility** means that, if all other parameters are kept constant, the solubility is a monotonically increasing function of pressure. In our research we showed that the solubility of gallium-containing nitride in supercritical nitrogen-containing solvents, such as ammonia, possesses a negative temperature coefficient and a positive pressure coefficient in temperatures ranging at least from 300 to 600°C and pressures from 1 to 5.5 kbar.

Over-saturation of supercritical solution with respect to gallium-containing nitride means that the concentration of gallium in a soluble form in said solution is higher than that in equilibrium (i.e. it is higher than solubility). In the case of dissolution of gallium-containing nitride in a closed system, such an over-saturation can be achieved by either increasing the temperature and/or decreasing the pressure.

Spontaneous crystallization means an undesired process where nucleation and growth of the gallium-containing nitride from over-saturated supercritical solution take place at any site within an autoclave except at the surface of a crystallization seed where the growth is desired. Spontaneous crystallization also comprises nucleation and disoriented growth on the surface of crystallization seed.

Selective crystallization on a seed means a process of crystallization on a seed carried out without spontaneous crystallization.

Autoclave means a closed container which has a reaction chamber where the ammonobasic process according to the present invention is carried out.

The present invention can provide a gallium-containing nitride monocrystal having a large size and a high quality. Such gallium-containing nitride crystals can have a surface area of more than 2 cm^2 and a dislocation density of less than $10^6 / \text{cm}^2$. Gallium-containing nitride crystals having a thickness of at least $200 \text{ }\mu\text{m}$ (preferably at least $500 \text{ }\mu\text{m}$) and a FWHM of 50 arcsec or less can also be obtained. Depending on the crystallization conditions, it is possible to obtain gallium-containing nitride crystals having a volume of more than 0.05 cm^3 , preferably more than 0.1 cm^3 using the processes of the invention.

As was explained above, the gallium-containing nitride crystal is a crystal of nitride of gallium and optionally other element(s) of Group XIII (the numbering of the groups is given according to the IUPAC convention of 1989 throughout this application). These compounds can be represented by the formula $\text{Al}_x\text{Ga}_{1-x-y}\text{In}_y\text{N}$, wherein $0 \leq x < 1$, $0 \leq y < 1$, $0 \leq x+y < 1$ (preferably $0 \leq x < 0.5$ and $0 \leq y < 0.5$). Although in a preferred embodiment, the gallium-containing nitride is gallium nitride, in a further preferred embodiment part (e.g.

up to 50 mol.-%) of the gallium atoms can be replaced by one or more other elements of Group XIII (especially Al and/or In).

The gallium-containing nitride may additionally include at least one donor and/or at least one acceptor and/or at least one magnetic dopant e.g. to alter the optical, electrical and magnetic properties of the substrate. Donor dopants, acceptor dopants and magnetic dopants are well-known in the art and can be selected according to the desired properties of the substrate. Preferably the donor dopants are selected from the group consisting of Si and O. As acceptor donors Mg and Zn are preferred. Any known magnetic dopant can be included into the substrates of the present invention. A preferred magnetic dopant is Mn and possibly also Ni and Cr. The concentrations of the dopants are well-known in the art and depend on the desired end application of the nitride. Typically the concentrations of these dopants range from 10^{17} to 10^{21} / cm^3 . Instead of adding dopants as part of the feedstock into the autoclave, dopants can also be included into the gallium-containing nitride crystal from trace amounts of the autoclave material which dissolve during the process of the invention. For example, if the autoclave comprises a nickel alloy then nickel can be included into the gallium-containing nitride crystal.

Due to the preparation process the gallium-containing nitride crystal can also contain alkali elements, usually in an amount of more than about 0.1 ppm. Generally it is desired to keep the alkali elements content lower than 10 ppm, although it is difficult to specify what concentration of alkali metals in gallium-containing nitride has a disadvantageous influence on its properties.

It is also possible that halogens are present in the gallium-containing nitride. The halogens can be introduced either intentionally (as a component of the mineralizer) or unintentionally (from impurities of the mineralizer or the feedstock). It is usually desired to keep the halogen content of the gallium-containing nitride crystal in the range of about 0.1 ppm or less.

The process of the invention is a supercritical crystallization process, which includes at least two steps: a dissolution step at a first temperature and at a first pressure and a crystallization step at a second temperature and at a second pressure. Since generally high

pressures and/or high temperatures are involved, the process according to the invention is preferably conducted in an autoclave. The two steps (i.e. the dissolution step and the crystallization step) can either be conducted separately or can be conducted at least partially simultaneously in the same reactor.

5 For conducting the two steps separately, the process can be conducted in one single reactor but the dissolution step is conducted before the crystallization step. In this embodiment the reactor can have the conventional construction of a single chamber. The process of the invention in the two-step embodiment can be conducted using constant pressure and two different temperatures or using constant temperature and two different
10 pressures. It is also possible to use two different pressures and two different temperatures. The exact values of pressure and temperature should be selected depending on the feedstock, the specific nitride to be prepared and the solvent. Generally the pressure is in the range of 1 to 10 kbar, preferably 1 to 5.5 kbar and more preferably 1.5 to 3 kbar. The temperature is usually in the range of 100 °C to 800 °C, preferably 300 °C to 600 °C, more
15 preferably 400 °C to 550 °C. If two different pressures are employed, the difference in pressure should be from 0.1 kbar to 9 kbar, preferably from 0.2 kbar to 3 kbar. However, if the dissolution and crystallization are controlled by the temperature, the difference in temperature should be at least 1 °C, and preferably from 5 °C to 150 °C.

In a preferred embodiment, the dissolution step and the crystallization step are
20 conducted at least partially simultaneously in the same container. For such an embodiment the pressure is practically uniform within the container, while the temperature difference between the dissolution zone and crystallization zone should be at least 1 °C, and preferably is from 5 °C to 150 °C. Furthermore, the temperature difference between the dissolution zone and crystallization zone should be controlled so as to ensure chemical
25 transport in the supercritical solution, which takes place through convection.

A possible construction of a preferred container is given in Fig. 9. For conciseness and ease of understanding in the following, the process will be explained particularly with respect to this preferred embodiment. However, the invention can be conducted with different container constructions as long as the principles outlined in the specification and the claims are adhered to.

In a preferred embodiment of the invention, the process can be conducted in an apparatus comprising an autoclave 1 having an internal space and comprising at least one device 4, 5 for heating the autoclave to at least two zones having different temperatures, wherein the autoclave comprises a device which separates the internal space into a dissolution zone 13 and a crystallization zone 14 (hereinafter also referred to as "separating device" or "installation"). These two zones having different temperatures should preferably coincide with the dissolution zone 13 and the crystallization zone 14. The device which separates the internal space of the autoclave can be, for example, at least one baffle 12 having at least one opening 2. Examples are baffles having a central opening, circumferential openings or a combination thereof. The size of the opening(s) 2 should be large enough to allow transport between the zones but should be sufficiently small to maintain a temperature gradient in the reactor. The appropriate size of the opening(s) depends on the size and the construction of the reactor and can be easily determined by a person skilled in the art.

In one embodiment, two different heating devices can be employed, the position of which preferably corresponds to the dissolution zone 13 and the crystallization zone 14. However, it has been observed that transport of gallium in a soluble form from the dissolution zone 13 to the crystallization zone 14 can be further improved if a cooling means 6 is present between the first and the second heating devices and is located at approximately the position of the separating device. The cooling means 6 can be realized by liquid (e.g. water) cooling or preferably by fan cooling. The heating devices can be powered electrically, by either inductive or, preferably, by resistive heating means. Use of a heating – cooling – heating configuration gives wider possibilities in forming the desired temperature distribution within the autoclave. For example, it enables to obtain a low temperature gradients with in most of the crystallization zone 14 and a low temperature

gradient within most of the dissolution zone 13, while achieving a high temperature gradient in the region of the baffle 12.

When the process of the present invention is conducted a gallium-containing feedstock, an alkali metal-containing component, at least one crystallization seed and a
5 nitrogen-containing solvent are provided in at least one container. In the preferred apparatus described above, the gallium-containing feedstock 16 is placed in the dissolution zone 13 and the at least one crystallization seed 17 is placed in the crystallization zone 14. The alkali metal-containing component is also preferably placed in the dissolution zone. Then the nitrogen-containing solvent is added to the container, which
10 is then closed. Subsequently the nitrogen-containing solvent is brought into a supercritical state, e.g. by increasing pressure and/or heat.

In the present invention any materials containing gallium, which are soluble in the supercritical solvent under the conditions of the present invention, can be used as a gallium-containing feedstock. Typically the gallium-containing feedstock will be a
15 substance or mixture of substances, which contains at least gallium, and optionally alkali metals, other Group XIII elements, nitrogen, and/or hydrogen, such as metallic Ga, alloys and inter-metallic compounds, hydrides, amides, imides, amido-imides, azides. Suitable gallium-containing feedstocks can be selected from the group consisting of gallium nitride GaN, azides such as $\text{Ga}(\text{N}_3)_3$, imides such as $\text{Ga}_2(\text{NH})_3$, amido-imides such as
20 $\text{Ga}(\text{NH})\text{NH}_2$, amides such as $\text{Ga}(\text{NH}_2)_3$, hydrides such as GaH_3 , gallium-containing alloys, metallic gallium and mixtures thereof. Preferred feedstocks are metallic gallium and gallium nitride and mixtures thereof. Most preferably, the feedstock is metallic gallium and gallium nitride. If elements of Group XIII other than gallium are to be present in the gallium-containing nitride crystal, corresponding compounds or mixed compounds
25 including Ga and the other Group XIII element can be used. If the substrate is to contain dopants or other additives, precursors thereof can be added to the feedstock.

The form of the feedstock is not particularly limited and it can be in the form of one or more pieces or in the form of a powder. If the feedstock is in the form of a powder, care should be taken that individual powder particles are not transported from the dissolution zone to the crystallization zone, where they can cause irregular crystallization. It is
5 preferable that the feedstock is in one or more pieces and that the surface area of the feedstock is larger than that of the crystallization seed.

The nitrogen-containing solvent employed in the present invention must be able to form a supercritical fluid, in which gallium can be dissolved in the presence of alkali metal ions. Preferably the solvent is ammonia, a derivative thereof or mixtures thereof. An
10 example of a suitable ammonia derivative is hydrazine. Most preferably the solvent is ammonia. To reduce corrosion of the reactor and to avoid side-reactions, halogens e.g. in the form of halides are preferably not intentionally added into the container. Although traces of halogens may be introduced into the system in the form of unavoidable impurities of the starting materials, care should be taken to keep the amount of halogen as
15 low as possible. Due to the use of a nitrogen-containing solvent such as ammonia it is not necessary to include nitride compounds into the feedstock. Metallic gallium (or aluminium or indium) can be employed as the feedstock while the solvent provides the nitrogen required for the nitride formation.

It has been observed that the solubility of gallium-containing feedstock, such as
20 gallium and corresponding elements of Group XIII and/or their compounds, can be significantly improved by the presence of at least one type of alkali metal-containing component as a solubilization aid ("mineralizer"). Lithium, sodium and potassium are preferred as alkali metals, wherein sodium and potassium are more preferred. The mineralizer can be added to the supercritical solvent in elemental form or preferably in the
25 form of its compound (such as a salt). Generally the choice of the mineralizer depends on the solvent employed in the process. According to our investigations, alkali metal having a smaller ion radius can provide lower solubility of gallium-containing nitride in the supercritical solvent than that obtained with alkali metals having a larger ion radius. For example, if the mineralizer is in the form of a compound such as a salt, it is preferably in
30 the form of an alkali metal hydride such as MH , an alkali metal nitride such as M_3N , an

alkali metal amide such as MNH_2 , an alkali metal imide such as M_2NH or an alkali metal azide such as MN_3 (wherein M is an alkali metal). The concentration of the mineralizer is not particularly restricted and is selected so as to ensure adequate levels of solubility of both feedstock (the starting material) and gallium-containing nitride (the resulting product). It is usually in the range of 1 : 200 to 1 : 2, in the terms of the mols of the metal ion based on the mols of the solvent (molar ratio). In a preferred embodiment the concentration is from 1 : 100 to 1 : 5, more preferably 1 : 20 to 1 : 8 mols of the metal ion based on the mols of the solvent.

The presence of the alkali metal ions in the process can lead to alkali metal in the thus prepared substrates. It is possible that the amount of alkali metal is more than about 0.1 ppm, even more than 10 ppm. However, in these amounts the alkali metals do not detrimentally effect the properties of the substrates. It has been found that even at an alkali metal content of 500 ppm, the operational parameters of the substrate according to the invention are still satisfactory.

The dissolved feedstock crystallizes in the crystallization step under the low solubility conditions on the crystallization seed(s) which are provided in the container. The process of the invention allows bulk growth of monocrystalline gallium-containing nitride on the crystallization seed(s) and in particular leads to the formation of stoichiometric gallium-containing nitride in the form of a bulk monocrystalline layer on the crystallization seed(s).

Various crystals can be used as crystallization seeds in the present invention, however, it is preferred that the chemical and crystallographic constitution of the crystallization seeds is similar to those of the desired layer of bulk monocrystalline gallium-containing nitride. Therefore, the crystallization seed preferably comprises a crystalline layer of gallium-containing nitride. To facilitate crystallization of the dissolved feedstock, the dislocation density of the crystallization seed is preferably less than $10^6 / \text{cm}^2$. Suitable crystallization seeds generally have a surface area of $8 \times 8 \text{ mm}^2$ or more and thickness of 100 μm or more, and can be obtained e.g. by HVPE.

After the starting materials have been introduced into the container and the nitrogen-containing solvent has been brought into its supercritical state, the gallium-containing feedstock is at least partially dissolved at a first temperature and a first pressure, e.g. in the dissolution zone of an autoclave. Gallium-containing nitride crystallizes on the crystallization seed (e.g. in the crystallization zone of an autoclave) at a second temperature and at a second pressure while the nitrogen-containing solvent is in the supercritical state, wherein the second temperature is higher than the first temperature and/or the second pressure is lower than the first pressure. If the dissolution and the crystallization steps take place simultaneously in the same container, the second pressure is essentially equal to the first pressure.

This is possible since the solubility of gallium-containing nitride under the conditions of the present invention shows a negative temperature coefficient and a positive pressure coefficient in the presence of alkali metal ions. Without wishing to be bound by theory, it is postulated that the following processes occur. In the dissolution zone, the temperature and pressure are selected such that the gallium-containing feedstock is dissolved and the nitrogen-containing solution is undersaturated with respect to gallium-containing nitride. In the crystallization zone, the temperature and pressure are selected such that the solution, although it contains approximately the same concentration of gallium as in the dissolution zone, is over-saturated with respect to gallium-containing nitride. Therefore, crystallization of gallium-containing nitride on the crystallization seed occurs. This is illustrated in Figure 15. Due e.g. to the temperature gradient, pressure gradient, concentration gradient, different chemical or physical character of dissolved feedstock and crystallized product etc., gallium is transported in a soluble form from the dissolution zone to the crystallization zone. In the present invention this is referred to as "chemical transport" of gallium-containing nitride in the supercritical solution. It is postulated that the soluble form of gallium is a gallium complex compound with a Ga atom in the coordination center surrounded by ligands, such as NH_3 molecules or its derivatives, like NH_2^- , NH^{2-} , etc.

This theory is equally applicable for all gallium-containing nitrides, such as AlGa₂N₃, InGa₂N₃ and AlInGa₂N₃ as well as GaN (The mentioned formulas are only intended to give the components of the nitrides. It is not intended to indicate their relative amounts). In the case of nitrides other than gallium nitride aluminum and/or indium in a soluble form also
5 have to be present in the supercritical solution.

In a preferred embodiment of the invention, the gallium-containing feedstock is dissolved in at least two steps. In this embodiment, the gallium-containing feedstock generally comprises two kinds of starting materials which differ in solubility. The difference in solubility can be achieved chemically (e.g. by selecting two different
10 chemical compounds) or physically (e.g. by selecting two forms of the same compound having for example different surface areas, like microcrystalline powder and large crystals). In a preferred embodiment, the gallium-containing feedstock comprises two different chemical compounds such as metallic gallium and gallium nitride which dissolve at different rates. In a first dissolution step, the first component of the gallium-containing
15 feedstock is substantially completely dissolved at a dissolution temperature and at a dissolution pressure in the dissolution zone. The dissolution temperature and the dissolution pressure, which can be set only in the dissolution zone or preferably in the whole container, are selected so that the second component of the gallium-containing feedstock and the crystallization seed(s) remain substantially undissolved. This first
20 dissolution step results in an undersaturated or at most saturated solution (preferably undersaturated solution) with respect to gallium-containing nitride. For example, the dissolution temperature can be 100 °C to 350 °C, preferably from 150 °C to 300 °C. The dissolution pressure can be 0.1 kbar to 5 kbar, preferably from 0.1 kbar to 3 kbar.

Subsequently the conditions in the crystallization zone are set at a second
25 temperature and at a second pressure so that over-saturation with respect to gallium-containing nitride is obtained and crystallization of gallium-containing nitride occurs on the at least one crystallization seed. Simultaneously the conditions in the dissolution zone are set at a first temperature and at a first pressure (preferably equal to the second pressure) so that the second component of the gallium-containing feedstock is now
30 dissolved (second dissolution step). As explained above the second temperature is higher

than the first temperature and/or the second pressure is lower than the first pressure so that the crystallization can take advantage of the negative temperature coefficient of solubility and/or of the positive pressure coefficient of solubility. Preferably the first temperature is higher than the dissolution temperature. During the second dissolution step and the
5 crystallization step, the system should be in a stationary state so that the concentration of gallium in the supercritical solution remains substantially constant, i.e. approximately the same amount of gallium should be dissolved per unit of time as is crystallized in the same unit of time. This allows for the growth of gallium-containing nitride crystals of especially high quality and large size.

10 Typical pressures for the crystallization step and the second dissolution step are in the range of 1 to 10 kbar, preferably 1 to 5.5 kbar and more preferably 1.5 to 3 kbar. The temperature is generally in the range of 100 to 800°C, preferably 300 to 600°C, more preferably 400 to 550°C. The difference in temperature should be at least 1 °C, and is preferably from 5 °C to 150 °C. As explained above, the temperature difference between
15 the dissolution zone and crystallization zone should be controlled so as to ensure chemical transport in the supercritical solution, which takes place through convection.

In the process of the invention, the crystallization should take place selectively on the crystallization seed and not on a wall of the container. Therefore, the over-saturation extent with respect to the gallium-containing nitride in the supercritical solution in the
20 crystallization zone should be controlled so as to be below the spontaneous crystallization level where crystallization takes place on a wall of the autoclave and/or disoriented growth occurs on the seed, i.e. the level at which spontaneous crystallization occurs. This can be achieved by adjusting the chemical transport rate and/or the crystallization temperature and/or crystallization pressure. The chemical transport is related on the speed of a
25 convective flow from the dissolution zone to the crystallization zone, which can be controlled by the temperature difference between the dissolution zone and the crystallization zone, the size of the opening(s) of baffle(s) between the dissolution zone and the crystallization zone etc.

The performed tests showed that the best bulk monocrystalline gallium nitride obtained had a dislocation density close to $10^4/\text{cm}^2$ and simultaneously a FWHM of X-ray rocking curve from (0002) plane below 60 arcsec. These crystals possess an appropriate quality and durability for optical semiconductor devices. The gallium-containing nitride of
5 the present invention typically has a wurzite structure.

Feedstock material for use in the present invention can also be prepared using a method similar to those described above. The method involves the steps of:

- (i) providing a gallium-containing feedstock, an alkali metal-containing component, at least one crystallization seed and a nitrogen-containing solvent
10 in a container having at least one zone;
- (ii) subsequently bringing the nitrogen-containing solvent into a supercritical state;
- (iii) subsequently dissolving the gallium-containing feedstock (such as metallic gallium or aluminium or indium, preferably metallic gallium) at a dissolution temperature and at a dissolution pressure, whereby the gallium-containing
15 feedstock is substantially completely dissolved and the crystallization seed remains substantially undissolved so that an undersaturated solution with respect to gallium-containing nitride is obtained;
- (iv) subsequently setting the conditions in at least part of the container at a second temperature and at a second pressure so that over-saturation with respect to
20 gallium-containing nitride is obtained and crystallization of gallium-containing nitride occurs on the at least one crystallization seed;
wherein the second temperature is higher than the dissolution temperature.

In this embodiment the comments given above with respect to the individual components, process parameters, etc. also apply. Preferably during the crystallization step
25 in this embodiment the conditions in the whole container are set at the second temperature and the second pressure.

Gallium-containing nitride exhibits good solubility in a supercritical nitrogen-containing solvent (e.g. ammonia), provided alkali metals or their compounds, such as KNH_2 , are introduced into it. Fig. 1 shows the solubility of gallium-containing nitride in a

supercritical solvent versus pressure for temperatures of 400 and 500°C wherein the solubility is defined by the molar percentage: $S_m \equiv \text{GaN}^{\text{solvent}} : (\text{KNH}_2 + \text{NH}_3) \text{ } 100\%$. In the present case the solvent is supercritical ammonia containing KNH_2 in a molar ratio $x \equiv \text{KNH}_2 : \text{NH}_3$ equal to 0.07. For this case S_m should be a smooth function of only three parameters: temperature, pressure, and molar ratio of mineralizer (i.e. $S_m = S_m(T, p, x)$).
Small changes of S_m can be expressed as:

$$\Delta S_m \approx (\partial S_m / \partial T)|_{p,x} \Delta T + (\partial S_m / \partial p)|_{T,x} \Delta p + (\partial S_m / \partial x)|_{T,p} \Delta x,$$

where the partial differentials (e.g. $(\partial S_m / \partial T)|_{p,x}$) determine the behavior of S_m with variation of its parameters (e.g. T). In this specification the partial differentials are called "coefficients" (e.g. $(\partial S_m / \partial T)|_{p,x}$ is a "temperature coefficient of solubility" or "temperature coefficient").

The diagram shown in Fig. 1 illustrates that the solubility increases with pressure and decreases with temperature, which means that it possesses a negative temperature coefficient and a positive pressure coefficient. Such features allow obtaining a bulk monocrystalline gallium-containing nitride by dissolution in the higher solubility conditions, and crystallization in the lower solubility conditions. In particular, the negative temperature coefficient means that, in the presence of a temperature gradient, the chemical transport of gallium in a soluble form can take place from the dissolution zone having a lower temperature to the crystallization zone having a higher temperature.

The process according to invention allows the growth of bulk monocrystalline gallium-containing nitride crystals on the crystallization seed and leads in particular to the formation of stoichiometric gallium-containing nitride, obtained in the form of a bulk monocrystalline layer grown on a gallium-containing nitride crystallization seed. Since such a monocrystal is obtained in a supercritical solution that contains ions of alkali metals, it can contain alkali metals in a quantity higher than 0.1 ppm. Because it is desired to maintain a purely basic character of the supercritical solution, mainly in order to avoid corrosion of the apparatus, halides are preferably not intentionally introduced into the solvent. The process of the invention can also provide a bulk monocrystalline gallium-containing nitride crystal in which part of the gallium, e.g. from 5 to 50 mol-% may be

substituted by Al and/or In. Moreover, the bulk monocrystalline gallium-containing nitride crystal may be doped with donor and/or acceptor and/or magnetic dopants. These dopants can modify optical, electric and magnetic properties of the gallium-containing nitride crystal. With respect to the other physical properties, the bulk monocrystalline gallium-containing nitride crystal can have a dislocation density below $10^6/\text{cm}^2$, preferably below $10^5/\text{cm}^2$, or most preferably below $10^4/\text{cm}^2$. Besides, the FWHM of the X-ray rocking curve from (0002) plane can be below 600 arcsec, preferably below 300 arcsec, and most preferably below 60 arcsec. The best bulk monocrystalline gallium nitride obtained may have a dislocation density lower than $10^4/\text{cm}^2$ and simultaneously a FWHM of the X-ray rocking curve from (0002) plane below 60 arcsec.

Due to their good crystalline quality the gallium-containing nitride crystals obtained in the present invention may be used as a substrate material for optoelectronic semiconductor devices based on nitrides, in particular for laser diodes.

The following examples are intended to illustrate the invention and should not be construed as being limiting.

EXAMPLES

The dislocation density can be measured by the so-called EPD method (Etch Pit Density) and subsequent evaluation using a microscope

The FWHM of the X-ray rocking curve can be determined by X-ray diffraction analysis.

Since it is not possible to readily measure the temperature in an autoclave while in use under supercritical conditions, the temperature in the autoclave was estimated by the following method. The outside of the autoclave is equipped with thermocouples near the dissolution zone and the crystallization zone. For the calibration, additional thermocouples were introduced into the inside of the empty autoclave in the dissolution zone and the crystallization zone. The empty autoclave was then heated stepwise to various

temperatures and the values of the temperature of the thermocouples inside the autoclave and outside the autoclave were measured and tabulated. For example, if the temperature of the crystallization zone is determined to be 500 °C and the temperature of the dissolution zone is 400 °C inside the empty autoclave when the temperature measured by the outside thermocouples are 480 °C and 395 °C, respectively. It is assumed that under supercritical conditions the temperatures in the crystallization/dissolution zones will also be 500 °C/400 °C when temperatures of 480 °C/395 °C are measured by the outside thermocouples. In reality, the temperature difference between the two zones can be lower due to effective heat transfer through the supercritical solution.

10 Example 1

Two crucibles were placed into a high-pressure autoclave having a volume of 10.9 cm³. The autoclave was manufactured according to a known design [H. Jacobs, D. Schmidt, *Current Topics in Materials Science*, vol. 8, ed. E. Kaldis (North-Holland, Amsterdam, 1981), 381]. One of the crucibles contained 0.4 g of gallium nitride in the form of 0.1 mm thick plates produced by the HVPE method as feedstock, while the other contained a gallium nitride seed of a double thickness weighing 0.1 g. The seed was also obtained by the HVPE method. Further, 0.72 g of metallic potassium of 4N purity was placed in the autoclave, the autoclave was filled with 4.81g of ammonia and then closed. The autoclave was put into a furnace and heated to a temperature of 400°C. The pressure within the autoclave was 2 kbar. After 8 days the temperature was increased to 500°C, while the pressure was maintained at the 2 kbar level and the autoclave was maintained under these conditions for another 8 days (Fig. 2). As a result of this process, in which the dissolution and crystallization steps were separated in time, the feedstock was completely dissolved and the recrystallization of gallium nitride in the form of a layer took place on the partially dissolved seed. The two-sided monocrystalline layers had a total thickness of about 0.4 mm.

Example 2

Two crucibles were put into the above-mentioned high-pressure autoclave having a volume of 10.9 cm^3 . One of the crucibles contained 0.44 g of gallium nitride in the form of 0.1mm thick plates produced by the HVPE method as feedstock, and the other contained a
5 gallium nitride seed of a double thickness weighing 0.1g, also obtained by the HVPE method. Further, 0.82 g of metallic potassium of 4N purity was placed in the autoclave, the autoclave was filled with 5.43g of ammonia and then closed. The autoclave was put into a furnace and heated to a temperature of 500°C . The pressure within the autoclave was 3.5 kbar. After 2 days the pressure was lowered to 2 kbar, while the temperature was
10 maintained at the 500°C level and the autoclave was maintained under these conditions for another 4 days (Fig. 3). As a result of this process, the feedstock was completely dissolved and the recrystallization of gallium nitride took place on the partially dissolved seed. The two-sided monocrystalline layers had a total thickness of about 0.25 mm.

Example 3

15 Two crucibles were placed into the above-mentioned high-pressure autoclave having a volume of 10.9 cm^3 . One of the crucibles contained 0.3 g of the feedstock in the form of metallic gallium of 6N purity and the other contained a 0.1g gallium nitride seed obtained by the HVPE method. Further, 0.6 g of metallic potassium of 4N purity was placed in the autoclave; the autoclave was filled with 4 g of ammonia and then closed. The autoclave
20 was put into a furnace and heated to a temperature of 200°C . After 2 days the temperature was increased to 500°C , while the pressure was maintained at the 2 kbar level and the autoclave was maintained in these conditions for further 4 days (Fig. 4). As a result of this process, the feedstock was completely dissolved and the crystallization of gallium nitride took place on the seed. The two-sided monocrystalline layers had a total thickness of about
25 0.3 mm.

Example 4

This is an example of a process, in which the dissolution and crystallization steps take place simultaneously (recrystallization process). In this example and all the following an apparatus is used which is schematically shown in Fig. 9 and Fig. 10. The basic unit of the apparatus is the autoclave 1, which in this Example has a volume of 35.6 cm³. The autoclave 1 is equipped with an separating device 2 which allows for chemical transport of the solvent in the supercritical solution inside the autoclave 1. For this purpose, the autoclave 1 is put into a chamber 3 of a set of two furnaces 4 provided with heating devices 5 and a cooling device 6. The autoclave 1 is secured in a desired position with respect to the furnaces 4 by means of a screw-type blocking device 7. The furnaces 4 are mounted on a bed 8 and are secured by means of steel tapes 9 wrapped around the furnaces 4 and the bed 8. The bed 8 together with the set of furnaces 4 is rotationally mounted in base 10 and is secured in a desired angular position by means of a pin interlock 11. In the autoclave 1, placed in the set of furnaces 4, the convective flow of supercritical solution takes place as determined by the separating device 2. The separating device 2 is in the form of a horizontal baffle 12 having a circumferential opening. The baffle 12 separates the dissolution zone 13 from the crystallization zone 14 in the autoclave 1, and enables, together with the adjustable tilting angle of the autoclave 1, controlling of speed and type of convective flow. The temperature level of the individual zones in the autoclave 1 is controlled by means of a control system 15 operating the furnaces 4. In the autoclave 1, the dissolution zone 13 coincides with the low-temperature zone of the set of furnaces 4 and is located above the horizontal baffle 12 and the feedstock 16 is put into this zone 13. On the other hand, the crystallization zone 14 coincides with the high-temperature zone of the set of furnaces 4 and it is located below the horizontal baffle 12. The crystallization seed 17 is mounted in this zone 14. The mounting location of the crystallization seed 17 is below the intersection of the rising and descending convective streams.

An amount of 3.0g of gallium nitride produced by the HVPE method was placed in the high-pressure autoclave described above, which was set in the horizontal position. This gallium nitride had the form of plates of about 0.2 mm thickness, and it was distributed

(roughly uniformly) in equal portions in the dissolution zone 13 and the crystallization zone 14. The portion placed in the dissolution zone 13 played the role of feedstock, whereas the portion placed in the crystallization zone 14 played the role of crystallization seeds. Metallic potassium of 4N purity was also added in a quantity of 2.4g. Then the
5 autoclave 1 was filled with 15.9g of ammonia (5N), closed, put into a set of furnaces 4 and heated to a temperature of 450°C. The pressure inside the autoclave 1 was approx. 2 kbar. During this stage, which lasted one day, partial dissolution of gallium nitride was carried out in both zones. Then the temperature of the crystallization zone 14 was increased to 500°C while the temperature of the dissolution zone 13 was lowered to 400°C and the
10 autoclave 1 was kept in these conditions for 6 more days (Fig. 5). As a final result of this process, partial dissolution of the feedstock in the dissolution zone 13 and crystallization of gallium nitride on the gallium nitride seeds in the crystallization zone 14 took place.

Example 5

The above-mentioned high pressure autoclave 1 having a volume of 35.6 cm³ was
15 charged with feedstock in the form of a 3.0g pellet of sintered gallium nitride (introduced into the dissolution zone 13), two seeds of gallium nitride obtained by the HVPE method and having the form of plates having a thickness of 0.4 mm and a total weight of 0.1g (introduced into the crystallization zone 14), as well as with 2.4g of metallic potassium of 4N purity. Then the autoclave was filled with 15.9g of ammonia (5N) and closed. The
20 autoclave 1 was then put into a set of furnaces 4 and heated to 450°C. The pressure inside the autoclave was about 2 kbar. After an entire day the temperature of the crystallization zone 14 was raised to 480°C, while the temperature of the dissolution zone 13 was lowered to 420°C and the autoclave was maintained under these conditions for 6 more days (see Fig. 6). As a result of the process the feedstock was partially dissolved in the dissolution
25 zone 13 and gallium nitride crystallized on the seeds in the crystallization zone 14. The two-sided monocrystalline layers had a total thickness of about 0.2 mm.

Example 6

The above-mentioned high pressure autoclave 1 having a volume of 35.6 cm³ (see Fig. 9) was charged with 1.6g of feedstock in the form of gallium nitride produced by the

HVPE method and having the form of plates having a thickness of about 0.2 mm (introduced into the dissolution zone 13), three gallium-nitride seeds of a thickness of about 0.35 mm and a total weight of 0.8g, also obtained by the HVPE method (introduced into the crystallization zone 14), as well as with 3.56 g of metallic potassium of 4N purity.

5 The autoclave 1 was filled with 14.5g of ammonia (5N) and closed. Then the autoclave 1 was put into a set of furnaces 4 and heated to 425°C. The pressure inside the autoclave was approx. 1.5 kbar. After an entire day the temperature of the dissolution zone 13 was lowered to 400°C while the temperature of the crystallization zone 14 was increased to 450°C and the autoclave was kept in these conditions for 8 more days (see Fig. 7). After

10 the process, the feedstock was found to be partially dissolved in the dissolution zone 13 and gallium nitride had crystallized on the seeds of the HVPE GaN in the crystallization zone 14. The two-sided monocrystalline layers had a total thickness of about 0.15 mm.

Example 7

The above-mentioned high pressure autoclave 1 having a volume of 35.6 cm³ (see

15 Fig. 9) was charged in its dissolution zone 13 with 2g of feedstock in the form of gallium nitride produced by the HVPE method and having the form of plates having a thickness of about 0.2 mm, and 0.47g of metallic potassium of 4N purity, and in its crystallization zone 14 with three GaN seeds of a thickness of about 0.3 mm and a total weight of about 0.3g also obtained by the HVPE method. The autoclave was filled with 16.5g of ammonia (5N)

20 and closed. Then the autoclave 1 was put into a set of furnaces 4 and heated to 500°C. The pressure inside the autoclave was approx. 3 kbar. After an entire day the temperature in the dissolution zone 13 was reduced to 450°C while the temperature in the crystallization zone 14 was raised to 550°C and the autoclave was kept under these conditions for the next 8 days (see Fig. 8). After the process, the feedstock was found to be partially dissolved in the

25 dissolution zone 13 and gallium nitride had crystallized on the seeds in the crystallization zone 14. The two-sided monocrystalline layers had a total thickness of about 0.4 mm.

Example 8

An amount of 1.0g of gallium nitride produced by the HVPE method was put into the dissolution zone 13 of the high-pressure autoclave 1 having a volume of 35.6 cm³. In the crystallization zone 14 of the autoclave, a crystallization seed of gallium nitride having a thickness of 100 μm and a surface area of 2.5 cm², obtained by the HVPE method, was placed. Then the autoclave was charged with 1.2 g of metallic gallium of 6N purity and 2.2 g of metallic potassium of 4N purity. Subsequently, the autoclave 1 was filled with 15.9g of ammonia (5N), closed, put into a set of furnaces 4 and heated to a temperature of 200°C. After 3 days – during which period metallic gallium was dissolved in the supercritical solution – the temperature was increased to 450°C which resulted in a pressure of about 2.3 kbar. The next day, the crystallization zone temperature was increased to 500°C while the temperature of the dissolution zone 13 was lowered to 370°C and the autoclave 1 was kept in these conditions for the next 20 days (see Fig. 11). As a result of this process, the partial dissolution of the material in the dissolution zone 13 and the growth of the gallium nitride on the gallium nitride seed in the crystallization zone 14 took place. The resulting crystal of gallium nitride having a total thickness of 350 μm was obtained in the form of two-sided monocrystalline layers.

Example 9

An amount of 3.0g of gallium nitride in the form of a sintered gallium nitride pellet was put into the dissolution zone 13 of high-pressure autoclave 1 having a volume of 35.6 cm³ (see Fig. 9). In the crystallization zone 14 of the autoclave, a crystallization seed of gallium nitride obtained by the HVPE method and having a thickness of 120 μm and a surface area of 2.2 cm² was placed. Then the autoclave was charged with 2.3 g of metallic potassium of 4N purity. Subsequently, the autoclave 1 was filled with 15.9g of ammonia (5N), closed, put into a set of furnaces 4 and heated to a temperature of 250°C in order to partially dissolve the sintered GaN pellet and obtain a preliminary saturation of a supercritical solution with gallium in a soluble form. After two days, the temperature of the crystallization zone 14 was increased to 500°C while the temperature of the dissolution zone 13 was lowered to 420°C and the autoclave 1 was kept in these conditions for the

next 20 days (see Fig. 12). As a result of this process, partial dissolution of the material in the dissolution zone 13 and growth of gallium nitride on the gallium nitride seed took place in the crystallization zone 14. A crystal of gallium nitride having a total thickness of 500 μm was obtained in the form of two-sided monocrystalline layers.

5 Example 10

An amount of 0.5g of gallium nitride plates having an average thickness of about 120 μm , produced by the HVPE method, were put into the dissolution zone 13 of high-pressure autoclave 1 having a volume of 35.6 cm^3 . In the crystallization zone 14 of the autoclave, three crystallization seeds of gallium nitride obtained by the HVPE method were placed. The crystallization seeds had a thickness of about 120 μm and a total surface area of 1.5 cm^2 . Then the autoclave was charged with 0.41 g of metallic lithium of 3N purity. Subsequently, the autoclave 1 was filled with 14.4g of ammonia (5N), closed, put into a set of furnaces 4 and heated so that the temperature of the crystallization zone 14 was increased to 550°C and the temperature of the dissolution zone 13 was increased to 450°C. The resulting pressure was about 2.6 kbar. The autoclave 1 was kept in these conditions for the next 8 days (see Fig. 13). As a result of this process, partial dissolution of the material in the dissolution zone 13 and growth of gallium nitride on the gallium nitride seeds in the crystallization zone 14 took place. The resulting crystals of gallium nitride had a thickness of 40 μm and were in the form of two-sided monocrystalline layers.

20 Example 11

An amount of 0.5g of gallium nitride having an average thickness of about 120 μm , produced by the HVPE method, was placed into the dissolution zone 13 of high-pressure autoclave 1 having a volume of 35.6 cm^3 . In the crystallization zone 14 of the autoclave, three crystallization seeds of gallium nitride obtained by the HVPE method were placed. The crystallization seeds had a thickness of 120 μm and a total surface area of 1.5 cm^2 . Then the autoclave was charged with 0.071 g of metallic gallium of 6N purity and 1.4 g of metallic sodium of 3N purity. Subsequently, the autoclave 1 was filled with 14.5g of ammonia (5N), closed, put into a set of furnaces 4 and heated to a temperature of 200°C. After 1 day – during which period metallic gallium was dissolved in the supercritical

solution – the autoclave 1 was heated so that the temperature in the crystallization zone was increased to 500°C, while the temperature in the dissolution zone was increased to 400°C. The resulting pressure was about 2.3 kbar. The autoclave 1 was kept in these conditions for the next 8 days (see Fig. 14). As a result of this process, partial dissolution
5 of the material in the dissolution zone 13 and growth of gallium nitride on the gallium nitride seeds in the crystallization zone 14 took place. The resulting crystals of gallium nitride were obtained in the form of two-sided monocrystalline layers having a total thickness of 400 µm.

Example 12

10 An amount of 0.5g of gallium nitride having an average thickness of about 120 µm, produced by the HVPE method, was placed into the dissolution zone 13 of the high-pressure autoclave 1 having a volume of 35.6 cm³. In the crystallization zone 14 of the autoclave, three crystallization seeds of gallium nitride obtained by the HVPE method were placed. The crystallization seeds had a thickness of 120 µm and a total surface area
15 of 1.5 cm². Then the autoclave was charged with 0.20 g of gallium amide and 1.4 g of metallic sodium of 3N purity. Subsequently, the autoclave 1 was filled with 14.6g of ammonia (5N), closed, put into a set of furnaces 4 and heated to a temperature of 200°C. After 1 day – during which period gallium amide was dissolved in the supercritical solution – the autoclave 1 was heated so that the temperature in the crystallization zone
20 was increased to 500°C, while the temperature in the dissolution zone was increased to 400°C. The resulting pressure was about 2.3 kbar. The autoclave 1 was kept in these conditions for the next 8 days (see also Fig. 14). As a result of this process, partial dissolution of the material in the dissolution zone 13 and growth of gallium nitride on the gallium nitride seeds in the crystallization zone 14 took place. The resulting crystals of
25 gallium nitride were in the form of two-sided monocrystalline layers having a total thickness of 490 µm.

Example 13

One crucible was placed into the above-mentioned high-pressure autoclave having a volume of 10.9 cm^3 . The crucible contained 0.3 g of the feedstock in the form of metallic gallium of 6N purity. Also three gallium-nitride seeds having a thickness of about 0.5mm and a total mass of 0.2g, all obtained by the HVPE method, were suspended within the autoclave. Further, 0.5 g of metallic sodium of 3N purity was placed in the autoclave; the autoclave was filled with 5.9 g of ammonia and then closed. The autoclave was put into a furnace and heated to a temperature of 200°C , where the pressure was about 2.5 kbar. After 1 day the temperature was increased to 500°C , while the pressure increased up to 5 kbar and the autoclave was maintained in these conditions for further 2 days (Fig. 16). As a result of this process, the feedstock was completely dissolved and crystallization of gallium nitride took place on the seed. The average thickness of the two-side-overgrown ~~monocrystalline layer of gallium nitride was about 0.14 mm. The FWHM of the X-ray~~ rocking curve from the (0002) plane at the gallium-terminated side was 43 arcsec, while at the nitrogen-terminated side it was 927 arcsec.

The monocrystalline gallium nitride layers have a wurzite structure like in all of the other examples.

CLAIMS

1. A process for obtaining a gallium-containing nitride crystal, comprising the steps of:
 - (i) providing a gallium-containing feedstock, an alkali metal-containing component, at least one crystallization seed and a nitrogen-containing solvent in at least one container;
 - (ii) bringing the nitrogen-containing solvent into a supercritical state;
 - (iii) at least partially dissolving the gallium-containing feedstock at a first temperature and at a first pressure; and
 - 10 (iv) crystallizing gallium-containing nitride on the crystallization seed at a second temperature and at a second pressure while the nitrogen-containing solvent is in the supercritical state;

wherein at least one of the following criteria is fulfilled:

 - (a) the second temperature is higher than the first temperature; and
 - 15 (b) the second pressure is lower than the first pressure.
2. The process according to claim 1, wherein the at least one container is an autoclave.
3. The process according to claim 1, wherein the gallium-containing feedstock is at least partially dissolved before step (iv).
4. The process according to claim 1, wherein the gallium-containing feedstock is at least partially dissolved during step (iv).
- 20 5. The process according to claim 1, wherein the process is conducted in a container having a dissolution zone at the first temperature and a crystallization zone at the second temperature and wherein the second temperature is higher than the first temperature.
- 25 6. The process according to claim 5, wherein the difference in temperature between the dissolution zone and crystallization zone is selected so as to ensure convective transport in the supercritical solution.

7. The process according to claim 6, wherein the difference in temperature between the second temperature and the first temperature is at least 1 °C.
8. The process according to claim 7, wherein the difference in temperature between the second temperature and the first temperature is from about 5 to about 150 °C.
- 5 9. The process according to claim 1, wherein the gallium-containing nitride has the general formula $Al_xGa_{1-x-y}In_yN$, where $0 \leq x < 1$, $0 \leq y < 1$, and $0 \leq x + y < 1$.
10. The process according to claim 9, wherein the gallium-containing nitride has the general formula $Al_xGa_{1-x-y}In_yN$, where $0 \leq x < 0.5$ and $0 \leq y < 0.5$.
- 10 11. The process according to claim 9, wherein the gallium-containing nitride is gallium nitride.

12. The process according to claim 1, wherein the gallium-containing nitride further contains at least one donor dopant, at least one acceptor dopant, at least one magnetic dopant or mixtures thereof.
13. The process according to claim 1, wherein the gallium-containing feedstock
15 comprises at least one compound selected from the group consisting of gallium nitride, gallium azides, gallium imides, gallium amido-imides, gallium hydrides, gallium-containing alloys, metallic gallium and mixtures thereof.
14. The process according to claim 13, wherein the gallium-containing feedstock comprises metallic gallium and gallium nitride.
- 20 15. The process according to claim 13, wherein the feedstock further comprises an aluminium feedstock, an indium feedstock or mixtures thereof, wherein the feedstocks are selected from the group consisting of nitrides, azides, imides, amido-imides, hydrides, alloys, metallic aluminium, and metallic indium.
- 25 16. The process according to claim 1, wherein the alkali metal-containing component is at least one metallic alkali metal or at least one alkali metal salt.

17. The process according to claim 16, wherein the alkali metal in the alkali metal-containing component is lithium, sodium, potassium or cesium.
18. The process according to claim 17, wherein the alkali metal in the alkali metal-containing component is sodium or potassium.
- 5 19. The process according to claim 16, wherein the alkali metal salt is an amide, an imide or an azide.
20. The process according to claim 1, wherein a surface of the at least one crystallization seed is a crystalline layer of a gallium-containing nitride.
21. The process according to claim 20, wherein the gallium-containing nitride of the
10 crystalline layer has the general formula $Al_xGa_{1-x-y}In_yN$, where $0 \leq x < 1$, $0 \leq y < 1$, and $0 \leq x+y < 1$.
22. The process according to claim 20, wherein the crystalline layer has a dislocation density of less than $10^6 / \text{cm}^2$.
23. The process according to claim 1, wherein the nitrogen-containing solvent is
15 ammonia, a derivative thereof, or mixtures thereof.
24. The process according to claim 1, wherein the first temperature and the second temperature are from about 100 °C to about 800 °C and wherein the second temperature is at least 1 °C higher than the first temperature.
25. The process according to claim 24, wherein the first temperature and the second
20 temperature are from about 300 °C to about 600 °C.
26. The process according to claim 25, wherein the first temperature and the second temperature are from about 400 °C to about 550 °C.
27. The process according to claim 1, wherein the first pressure and the second pressure are the same and are from about 1000 bar (10^5 kPa) to about 10 000 bar (10^6 kPa).

28. The process according to claim 27, wherein the first pressure and the second pressure are the same and are from about 1000 bar (10^5 kPa) to about 5500 bar (5.5×10^5 kPa).
29. The process according to claim 28, wherein the first pressure and the second pressure are the same and are from about 1500 bar (1.5×10^5 kPa) to about 3000 bar (3×10^5 kPa).
30. The process according to claim 1, wherein step (iv) is conducted so that the crystallization selectively takes place on the crystallization seed.
31. A process for preparing a gallium-containing nitride crystal comprising the steps of:
- (i) providing a gallium-containing feedstock comprising at least two different components, an alkali metal-containing component, at least one crystallization seed and a nitrogen-containing solvent in a container having a dissolution zone and a crystallization zone, whereby the gallium-containing feedstock is provided in the dissolution zone and the at least one crystallization seed is provided in the crystallization zone;
 - (ii) subsequently bringing the nitrogen-containing solvent into a supercritical state;
 - (iii) subsequently partially dissolving the gallium-containing feedstock at a dissolution temperature and at a dissolution pressure in the dissolution zone, whereby a first component of the gallium-containing feedstock is substantially completely dissolved and a second component of the gallium-containing feedstock as well as the crystallization seed(s) remain substantially undissolved so that an undersaturated or saturated solution with respect to gallium-containing nitride is obtained;
 - (iv) subsequently setting the conditions in the crystallization zone at a second temperature and at a second pressure so that over-saturation with respect to gallium-containing nitride is obtained and crystallization of gallium-containing nitride occurs on the at least one crystallization seed and setting the conditions in the dissolution zone at a first temperature and at a first pressure so that the second component of the gallium-containing feedstock is dissolved;

wherein the second temperature is higher than the first temperature.

32. The process according to claim 31, wherein the first component of the gallium-containing feedstock is metallic gallium and the second component of the gallium-containing feedstock is gallium nitride.
- 5 33. The process according to claim 31, wherein the crystallization is conducted so that it selectively takes place on the crystallization seed.
34. The process according to claim 31, wherein the first temperature and the first pressure in the dissolution zone and the second temperature and the second pressure in the crystallization zone are selected so that the concentration of gallium in the
10 over-saturated solution remains substantially the same during crystallization.
35. The process according to claim 31, wherein the container comprises at least one baffle between the dissolution zone and the crystallization zone.
36. The process according to claim 35, wherein the at least one baffle has a central opening, circumferential openings or a combination thereof.
- 15 37. A gallium-containing nitride crystal obtainable by a process according to any one of claims 1 to 36.
38. A gallium-containing nitride crystal having a surface area of more than 2 cm^2 and having a dislocation density of less than $10^6 / \text{cm}^2$.
39. A gallium-containing nitride crystal having a thickness of at least $200 \text{ }\mu\text{m}$ and a full
20 width at half maximum (FWHM) of X-ray rocking curve from (0002) plane of 50 arcsec or less.
40. The gallium-containing nitride crystal according to claim 39 wherein the thickness is at least $500 \text{ }\mu\text{m}$.
41. The gallium-containing nitride crystal according to any of claims 37 to 40, wherein
25 the gallium-containing nitride crystal has the general formula $\text{Al}_x\text{Ga}_{1-x-y}\text{In}_y\text{N}$, where $0 \leq x < 1$, $0 \leq y < 1$, and $0 \leq x+y < 1$.

42. The gallium-containing nitride crystal according to any of claims 37 to 40, wherein the gallium-containing nitride crystal contains alkali elements in an amount of more than about 0.1 ppm.
- 5 43. The gallium-containing nitride crystal according to any of claims 37 to 40, wherein the gallium-containing nitride crystal has a halogen content of about 0.1 ppm or less.
44. The gallium-containing nitride crystal according to any of claims 37 to 40, wherein the gallium-containing nitride crystal has a volume of more than 0.05 cm³.
- 10 45. The gallium-containing nitride crystal according to any of claims 37 to 40, wherein the gallium-containing nitride crystal contains at least one element selected from the group consisting of Ti, Fe, Co, Cr, and Ni.
46. The gallium-containing nitride crystal according to any of claims 37 to 40, wherein the gallium-containing nitride crystal additionally contains at least one donor dopant and/or at least one acceptor dopant and/or at least one magnetic dopant in a concentration from 10¹⁷ to 10²¹ / cm³.
- 15 47. The gallium-containing nitride crystal according to any of claims 37 to 40, wherein the layer of gallium-containing nitride crystal further contains Al and/or In and the molar ratio of Ga to Al and/or In is more than 0.5.
48. The gallium-containing nitride crystal according to any of claims 37 to 40, wherein the gallium-containing nitride crystal contains a seed.
- 20 49. The gallium-containing nitride crystal according to any of claims 37 to 40, wherein the gallium-containing nitride crystal is monocrystalline.
- 25 50. An apparatus for obtaining a gallium-containing nitride crystal comprising an autoclave 1 having an internal space and comprising at least one device 4, 5 for heating the autoclave to at least two zones having different temperatures, wherein the autoclave comprises a device which separates the internal space into a dissolution zone 13 and a crystallization zone 14.

51. The apparatus according to claim 50, wherein the at least one device is for heating the autoclave to two zones having different temperatures and the two zones coincide with the dissolution zone 13 and the crystallization zone 14.
52. The apparatus according to claim 50, wherein the device which separates the internal space is at least one baffle 12 having at least one opening.
53. The apparatus according to claim 52, wherein the at least one baffle 12 has a central opening, circumferential openings or a combination thereof.
54. The apparatus according to claim 50, wherein the crystallization zone 14 is provided with a heating device 5 for heating the crystallization zone 14 to a temperature higher than the temperature of the dissolution zone 13.
55. The apparatus according to claim 50, wherein a seed-holder 18 is provided in the crystallization zone 14 and a feedstock-holder 19 is provided in the dissolution zone 13.
56. The apparatus according to claim 52, wherein the baffle(s) is/are in a horizontal position and wherein the dissolution zone 13 is located above said horizontal baffle or horizontal baffles 12, whereas said crystallization zone 14 is located below said horizontal baffle or horizontal baffles 12.
57. A process for obtaining a bulk monocrystalline gallium-containing nitride crystal, wherein it is performed in an autoclave, in the environment of a supercritical solvent containing ions of alkali metals, wherein a gallium-containing feedstock for making said gallium-containing nitride crystal becomes dissolved in said supercritical solvent to form a supercritical solution, and the gallium-containing nitride becomes crystallized from the supercritical solution on the surface of a crystallization seed at a temperature higher and/or pressure lower than that of the feedstock dissolution in the supercritical solvent.

58. The process according to claim 57, wherein said process comprises the steps of dissolving the gallium-containing feedstock and a separate step of transferring the supercritical solution to the higher temperature and/or to the lower pressure.
59. The process according to claim 57, wherein said process comprises the step of simultaneous creation of at least two zones of different temperatures, said gallium-containing feedstock is placed in the dissolution zone of the lower temperature, while the crystallization seed is placed in the crystallization zone of the higher temperature.
60. The process according to claim 59, wherein said temperature difference between said dissolution zone and said crystallization zone is controlled so as to ensure chemical transport in the supercritical solution.
61. The process according to claim 60, wherein said chemical transport in the supercritical solution takes place through convection in the autoclave.
62. The process according to claim 60, wherein said temperature difference between the dissolution zone and the crystallization zone is greater than 1°C.
63. The process according to claim 57, wherein said gallium-containing nitride crystal has the formula $\text{Al}_x\text{Ga}_{1-x-y}\text{In}_y\text{N}$, where $0 \leq x < 1$, $0 \leq y < 1$, $0 \leq x+y < 1$.
64. The process according to claim 57, wherein said gallium-containing nitride crystal contains dopants of a donor and/or acceptor and/or magnetic type.
65. The process according to claim 57, wherein said supercritical solvent contains NH_3 and/or its derivatives.
66. The process according to claim 57, wherein said supercritical solvent contains sodium and/or potassium ions.
67. The process according to claim 57, wherein said gallium-containing feedstock consists essentially of gallium-containing nitride and/or its precursors.

- 5 68. The process according to claim 67, wherein said precursors are selected from the group consisting of gallium azides, gallium imides, gallium amido-imides, gallium amides, gallium hydrides, gallium-containing alloys, and metallic gallium and optionally corresponding compounds of other elements of Group XIII (according to IUPAC, 1989).
69. The process according to claim 57, wherein said crystallization seed has at least a crystalline layer of gallium-containing nitride.
- 10 70. The process according to claim 57, wherein said crystallization seed has at least a crystalline layer of gallium-containing nitride with a dislocation density below $10^6/\text{cm}^2$.
71. The process according to claim 57, wherein said crystallization of a gallium-containing nitride takes place at a temperature from 100 to 800°C, preferably 300 to 600°C, more preferably 400 to 550°C.
- 15 72. The process according to claim 57, wherein said crystallization of a gallium-containing nitride takes place at a pressure from 100 to 10000 bar, preferably 1000 to 5500 bar, more preferably 1500 to 3000 bar.
73. The process according to claim 57, wherein the content of alkali metal ions in the supercritical solvent is controlled so as to provide adequate levels of solubility of said feedstock as well as of said gallium-containing feedstock.
- 20 74. The process according to claim 57, wherein the molar ratio of the moles of said alkali metal ions to the moles of the supercritical solvent is controlled within the range of 1:200 to 1:2, preferably 1:100 to 1:5, more preferably 1:20 to 1:8.
- 25 75. An apparatus for obtaining of a monocrystalline gallium-containing nitride crystal, comprising an autoclave 1 for producing supercritical solvent, equipped with an installation 2 for establishing a convective flow, the autoclave being mounted inside a furnace or set of furnaces 4 which are equipped with heating devices 5 and/or cooling devices 6.

76. The apparatus according to claim 75, wherein said furnace or set of furnaces 4 has a high-temperature zone coinciding with the crystallization zone 14 of said autoclave 1 equipped with heating devices 5, and a low-temperature zone coinciding with the dissolution zone 13 of the autoclave 1 equipped with heating devices 5 and/or cooling devices 6.
77. The apparatus according to claim 76, wherein said furnace or set of furnaces 4 has a high-temperature zone coinciding with the crystallization zone 14 of said autoclave 1 equipped with heating devices 5 and/or cooling devices 6, as well as a low-temperature zone coinciding with the dissolution zone 13 of the autoclave 1 equipped with heating devices 5 and/or cooling devices 6.
78. The apparatus according to claim 76, wherein said installation 2 is in the form of a horizontal baffle or horizontal baffles 12 having central and/or circumferential openings, separating the crystallization zone 14 from the dissolution zone 13.
79. The apparatus according to claim 76, wherein feedstock 16 is placed in the autoclave 1 in the dissolution zone 13, and said a crystallization seed 17 is placed in the crystallization zone 14, and said convective flow between the zones 13 and 14 is established by said installation 2.
80. The apparatus according to claim 79, wherein said dissolution zone 13 is located above said horizontal baffle or horizontal baffles 12, whereas said crystallization zone 14 is located below said horizontal baffle or horizontal baffles 12.
81. A process for preparing a bulk monocrystalline gallium-containing nitride crystal in an autoclave, which comprises the steps of (i) providing a supercritical ammonia solution containing ions of alkali metal and gallium in a soluble form by introducing a gallium-containing feedstock to supercritical ammonia solvent containing ions of alkali metals, in which solubility of gallium-containing nitride shows a negative temperature coefficient in said supercritical ammonia solution, and (ii) crystallizing said gallium-containing nitride selectively on a crystallization seed from said

supercritical ammonia solution by means of the negative temperature coefficient of solubility.

82. A process for preparing a bulk monocrystalline gallium-containing nitride in an autoclave, which comprises the steps of (i) providing a supercritical ammonia solution containing ions of alkali metal and gallium in a soluble form by introducing
5 a gallium-containing feedstock into a supercritical ammonia solvent containing ions of alkali metals, in which solubility of gallium-containing nitride shows a positive pressure coefficient in said supercritical ammonia solution, and (ii) crystallizing said gallium-containing nitride selectively on a crystallization seed from said
10 supercritical ammonia solution by means of the positive pressure coefficient of solubility.
83. A process for preparing a bulk monocrystalline gallium-containing nitride in an autoclave according to Claim 81 or 82, wherein said gallium-containing nitride is GaN.
- 15 84. A process for preparing a bulk monocrystalline gallium-containing nitride in an autoclave according to Claim 81 or 82, wherein said ion of alkali metal is selected from the group consisting of Li^+ , Na^+ , and K^+ .
85. A process for preparing a bulk monocrystalline gallium-containing nitride in an autoclave according to Claim 81 or 82, wherein said ions of alkali metals are
20 introduced in the form of mineralizers selected from alkali metals and compounds thereof, such as azides, nitrides, amides, amido-imides, imides, and/or hydrides, for forming an ammono-basic supercritical ammonia solution, which does not contain ions of halogens.
86. A process for preparing a bulk monocrystalline gallium-containing nitride in an autoclave according to Claim 81 or 82, wherein said gallium-containing nitride is
25 dissolved in said supercritical ammonia solvent in the form of gallium complex compounds containing alkali metals and NH_3 and/or its derivatives.

87. A process for preparing a bulk monocrystalline gallium-containing nitride in an autoclave according to Claim 81 or 82, wherein said gallium complex compound in said supercritical ammonia solution is formed from a dissolution of GaN and/or dissolution of metallic Ga with supercritical ammonia solvent.
- 5 88. A process for preparing a supercritical ammonia solution containing gallium-containing nitride, which comprises the steps of (i) providing a supercritical ammonia solvent by means of adjusting a temperature and/or pressure in an autoclave and (ii) dissolving a precursor of gallium-containing nitride in said supercritical ammonia solvent to form soluble gallium complex compounds at a
10 temperature lower than that at which dissolving of gallium-containing nitride takes place effectively.
89. A process for preparing a supercritical ammonia solution containing gallium-containing nitride according to claim 88, wherein the step of dissolving said precursor in said supercritical ammonia solvent is carried out at a temperature of 150
15 to 300°C.
90. A process for controlling the recrystallization of a gallium-containing nitride in a supercritical ammonia solution, which comprises the steps of (i) preparing a supercritical ammonia solution containing soluble gallium complex compound formed by dissolving of gallium-containing nitride feedstock in an autoclave and (ii)
20 decreasing the solubility of said gallium-containing nitride in the supercritical ammonia solution by increasing the temperature above that at which dissolving of the gallium-containing nitride feedstock is carried out.
91. A process for controlling the recrystallization of a gallium-containing nitride in a supercritical ammonia solution which comprises the steps of preparing a
25 supercritical ammonia solution containing soluble gallium complex compounds formed by dissolving of gallium-containing nitride feedstock in the dissolution zone and (ii) controlling over-saturation of said supercritical ammonia solution with respect to the crystallization seed, while maintaining a temperature in the crystallization zone lower than that in the dissolution zone.

- 5 92. A process for controlling recrystallization of a gallium-containing nitride in a supercritical ammonia solution according to claim 91, in which over-saturation of said supercritical solution with respect to said crystallization seed is maintained below the level where the phenomenon of spontaneous nucleation of gallium-containing nitride appears.
- 10 93. A process for controlling recrystallization of a gallium-containing nitride in a supercritical ammonia solution according to claim 91, in which over-saturation of said supercritical ammonia solution with respect to said crystallization seed, is controlled by adjusting pressure and composition of the supercritical ammonia solvent.
- 15 94. A process for controlling recrystallization of a gallium-containing nitride in a supercritical ammonia solution according to claim 91, in which over-saturation of said supercritical ammonia solution is controlled by adjusting the crystallization temperature.
- 20 95. A process for controlling recrystallization of a gallium-containing nitride in a supercritical ammonia solution according to claim 91, in which over-saturation of said supercritical ammonia solution is controlled by adjusting the temperature difference between the dissolution zone and the crystallization zone.
- 25 96. A process for controlling recrystallization of a gallium-containing nitride in a supercritical ammonia solution according to claim 91, in which over-saturation of said supercritical ammonia solution is controlled by adjusting the rate of chemical transport.
97. A process for controlling recrystallization of a gallium-containing nitride in a supercritical ammonia solution according to claim 90, in which controlling solubility of said gallium-containing nitride in the supercritical ammonia solution is carried out by adjusting the convective flow between the dissolution zone and the crystallization zone.

98. A process for controlling recrystallization of a gallium-containing nitride in a supercritical ammonia solution according to claim 90, in which controlling solubility of said gallium-containing nitride in the supercritical ammonia solution is carried out by adjusting the opening ratio of a baffle or baffles between the dissolution zone and the crystallization zone.
99. Substrate for epitaxy crystallized on the surface of a crystallization seed, especially a substrate for nitride semiconductor layers, wherein the substrate has a layer of bulk monocrystalline gallium-containing nitride, has a surface area of more than 2 cm^2 and has a dislocation density of less than $10^6 / \text{cm}^2$.
100. Substrate for epitaxy according to claim 99, wherein the layer of bulk monocrystalline gallium-containing nitride has the general formula $\text{Al}_x\text{Ga}_{1-x-y}\text{In}_y\text{N}$, where $0 \leq x < 1$, $0 \leq y < 1$, and $0 \leq x + y < 1$.
101. Substrate for epitaxy according to claim 99, wherein the substrate contains alkali elements in an amount of more than about 0.1 ppm.
102. Substrate for epitaxy according to claim 99, wherein the layer of bulk monocrystalline gallium-containing nitride has a halogen content that does not exceed about 0.1 ppm.
103. Substrate for epitaxy according to claim 99, wherein the layer of bulk monocrystalline gallium-containing nitride has volume of more than 0.05 cm^3 .
104. Substrate for epitaxy according to claim 99, wherein in the layer of bulk monocrystalline gallium-containing nitride has a full width at half maximum (FWHM) of X-ray rocking curve from (0002) plane of less than 600 arcsec.
105. Substrate for epitaxy according to claim 99, wherein the layer of bulk monocrystalline gallium-containing nitride additionally contains at least one donor dopant and/or at least one acceptor dopant and/or at least one magnetic dopant in a concentration from 10^{17} to $10^{21} / \text{cm}^3$.

106. Substrate for epitaxy according to claim 99, wherein the layer of bulk monocrystalline gallium-containing nitride contains Al and/or In and the molar ratio of Ga to Al and/or In is more than 0.5.
- 5 107. Substrate for epitaxy according to claim 99, wherein the layer of bulk monocrystalline gallium-containing nitride is crystallized on the surface of a crystallization seed of gallium-containing nitride having a dislocation density of less than $10^6 / \text{cm}^2$.
- 10 108. Substrate for epitaxy according to claim 99, wherein the layer of bulk monocrystalline gallium-containing nitride has a dislocation density of less than $10^4 / \text{cm}^2$ and a full width at half maximum (FWHM) of X-ray rocking curve from (0002) plane of less than 60 arcsec.

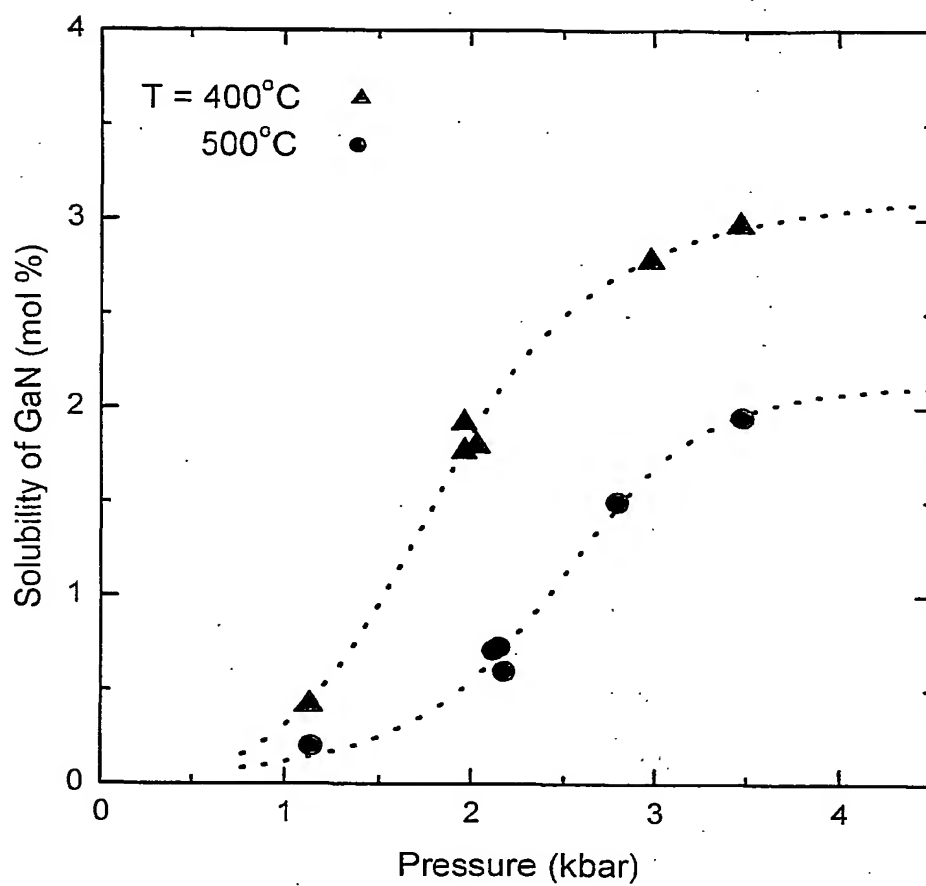


Fig. 1

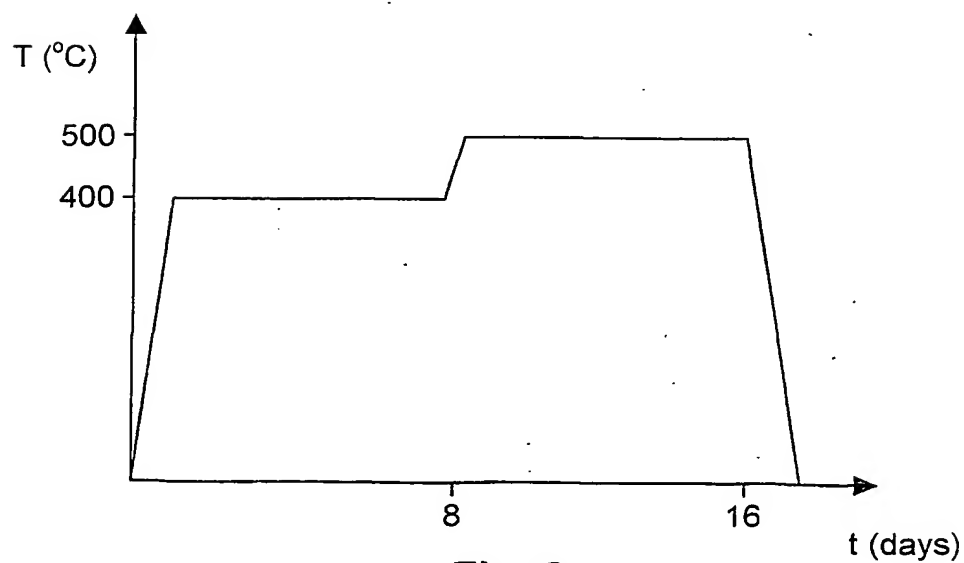


Fig. 2

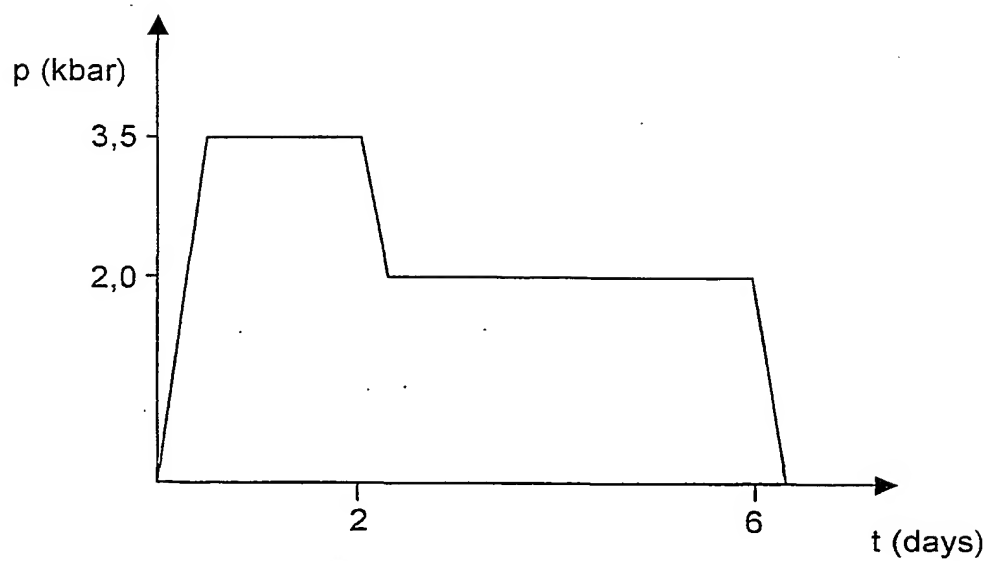


Fig. 3

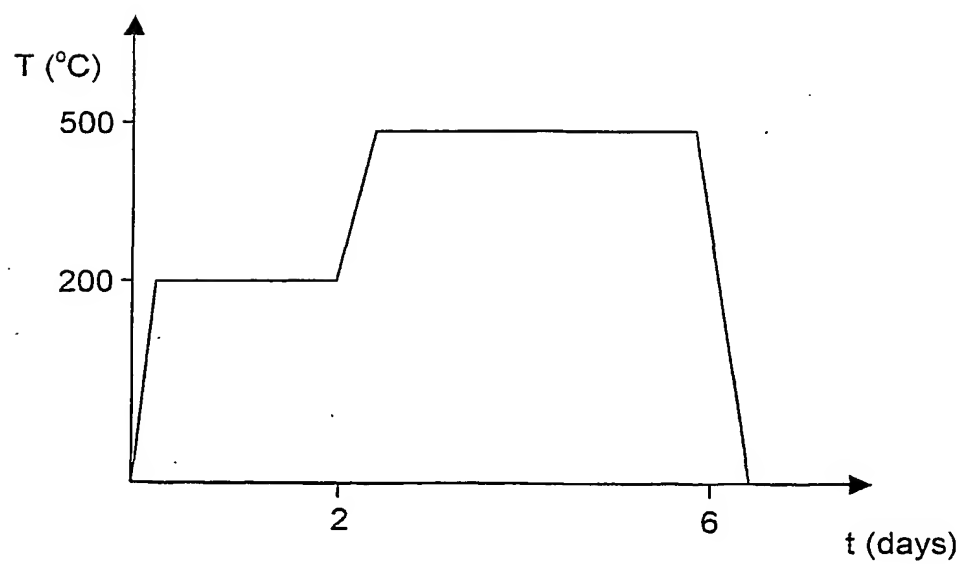


Fig. 4

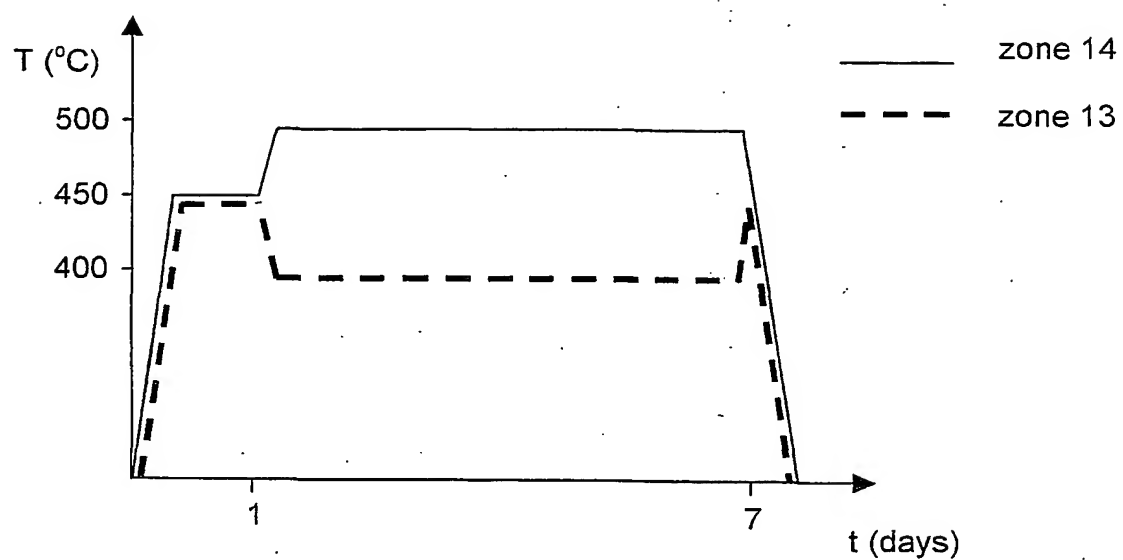


Fig. 5

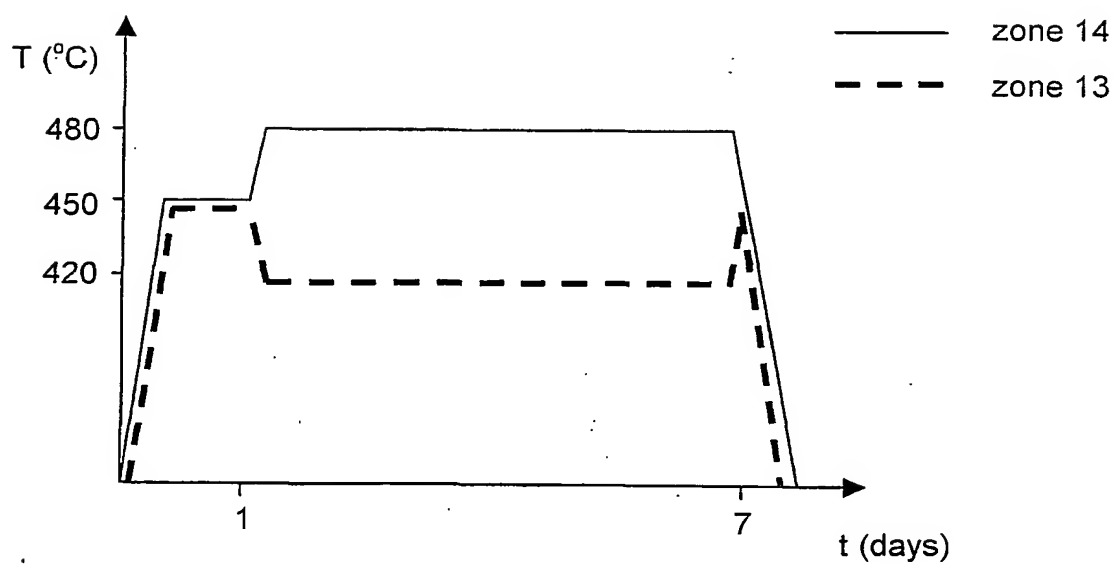


Fig. 6

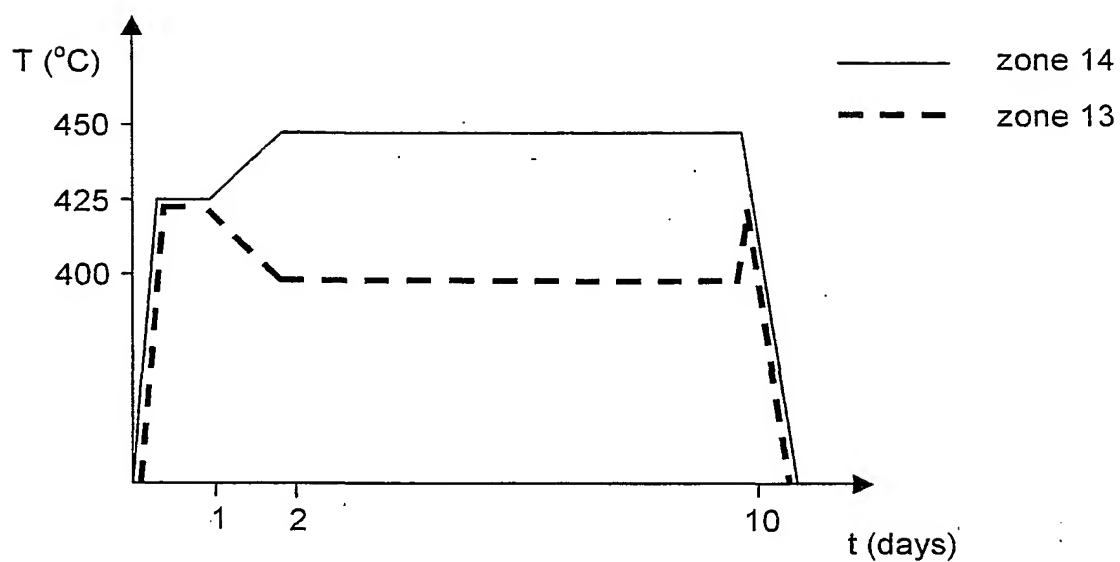


Fig. 7

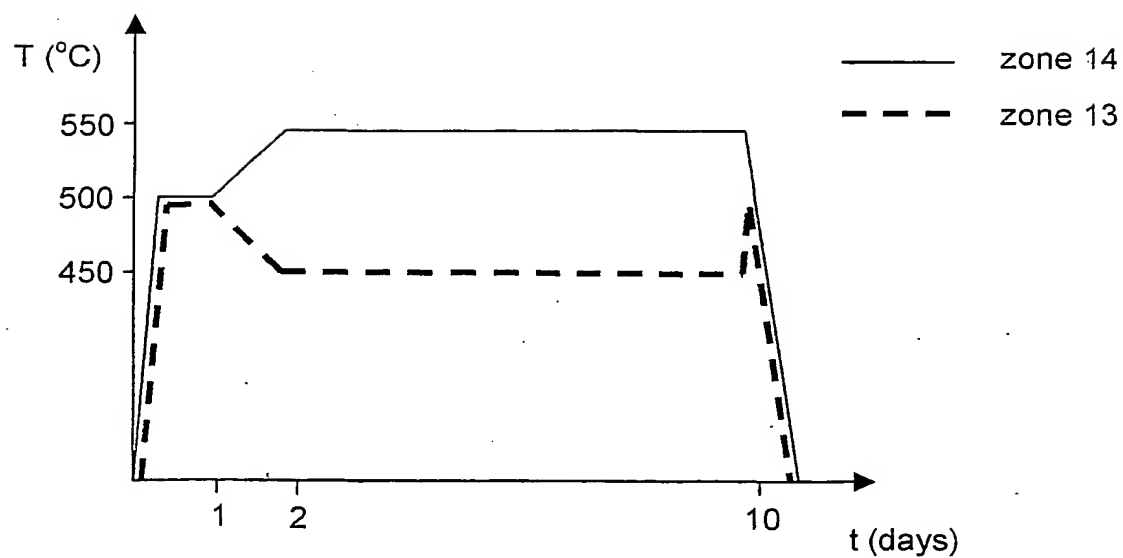
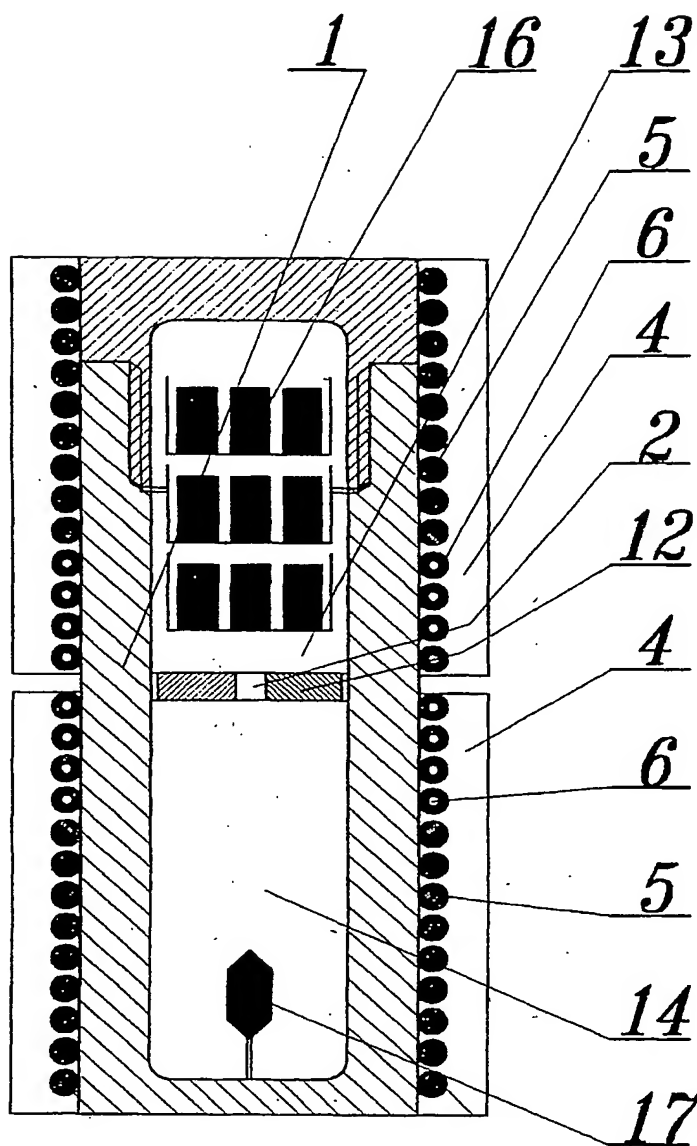


Fig. 8

*Fig. 9*

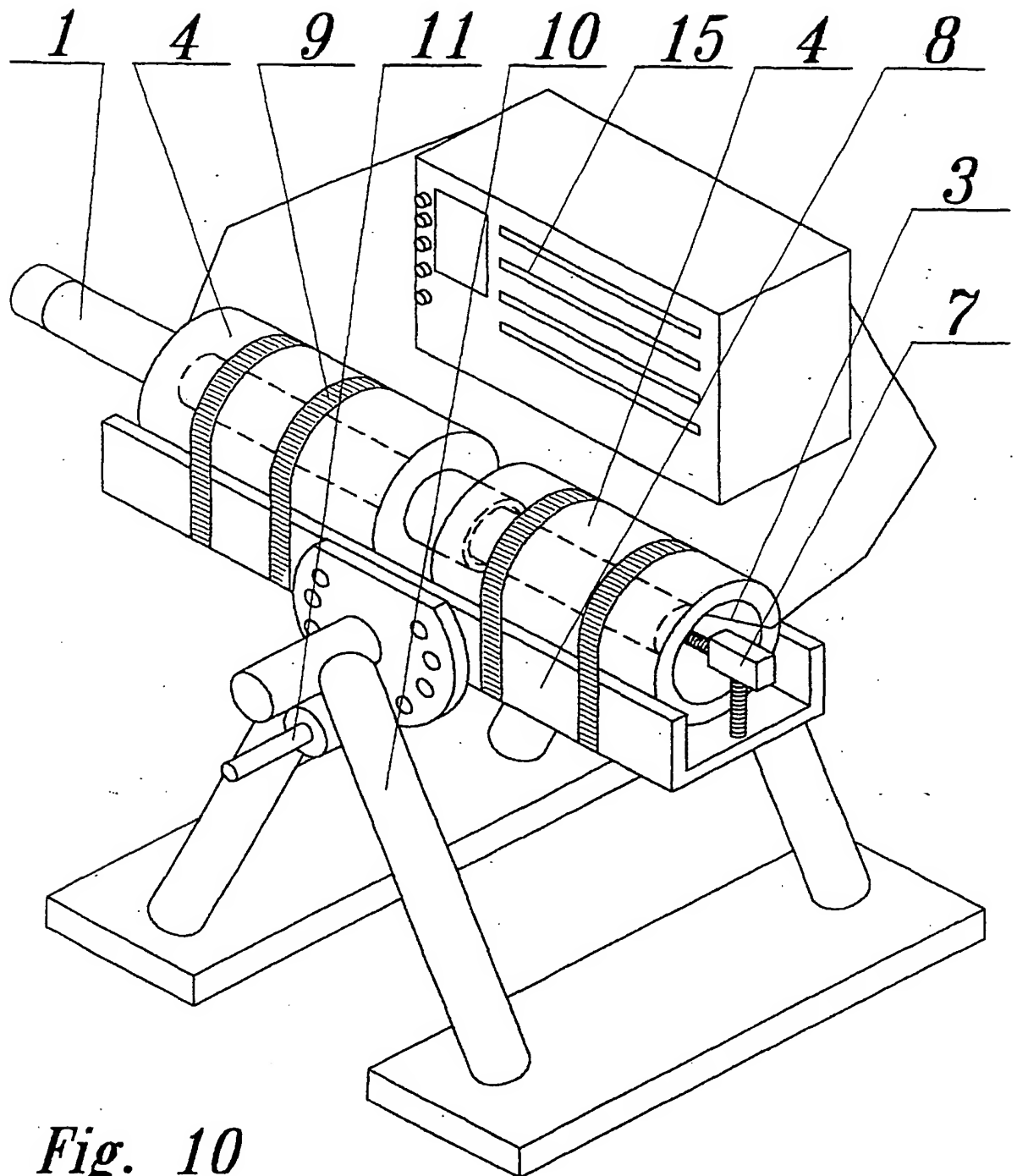


Fig. 10

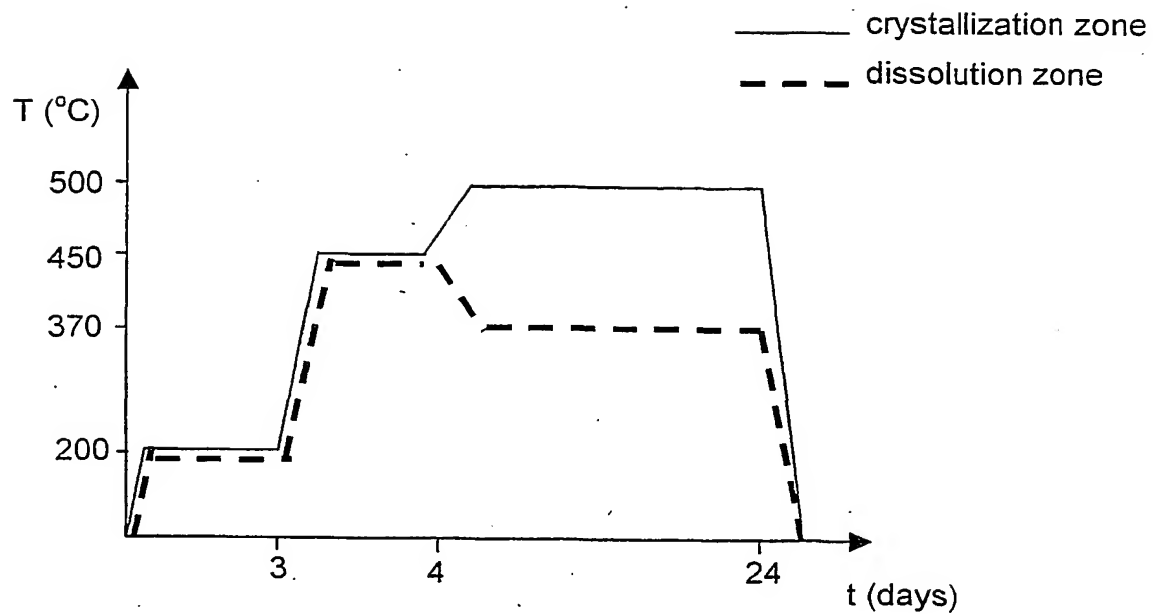


Fig. 11

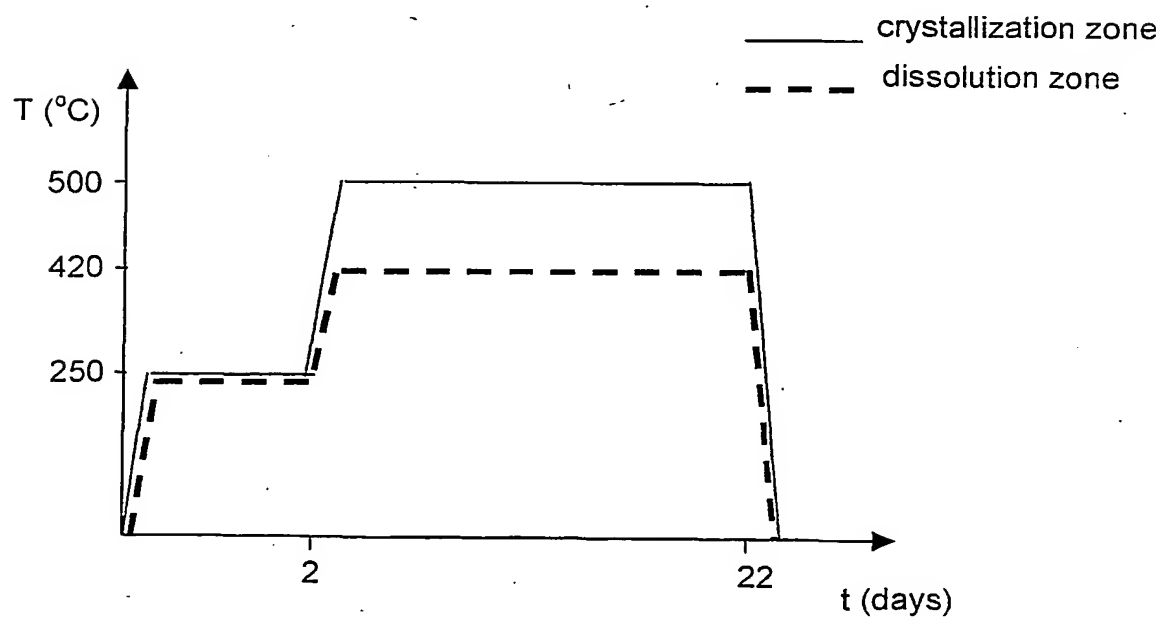


Fig. 12

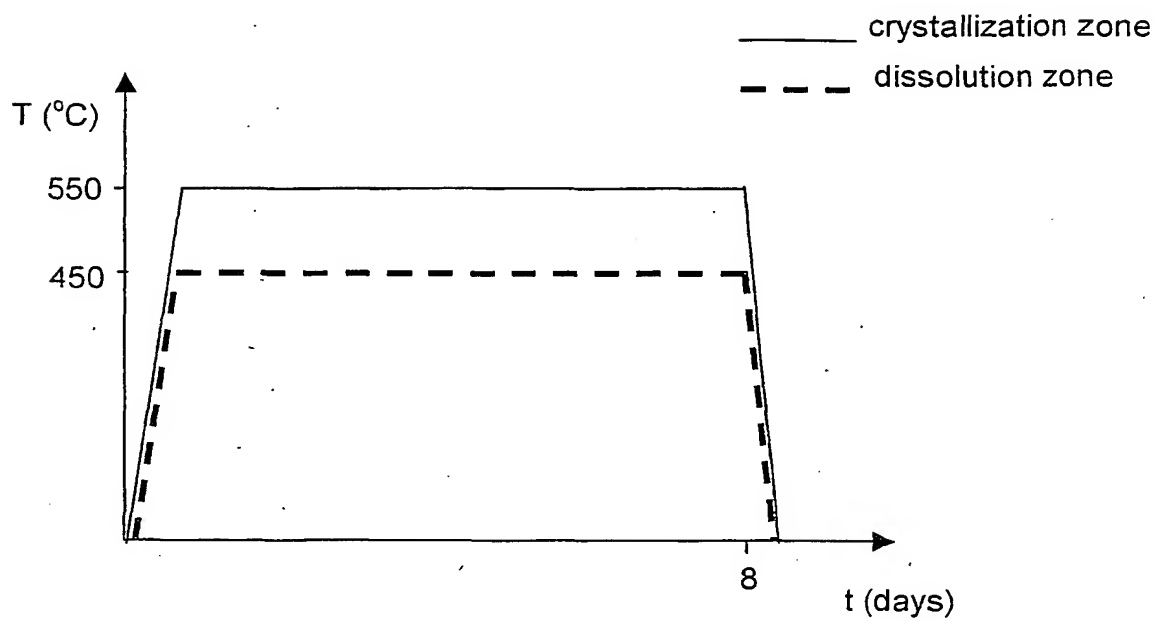


Fig. 13

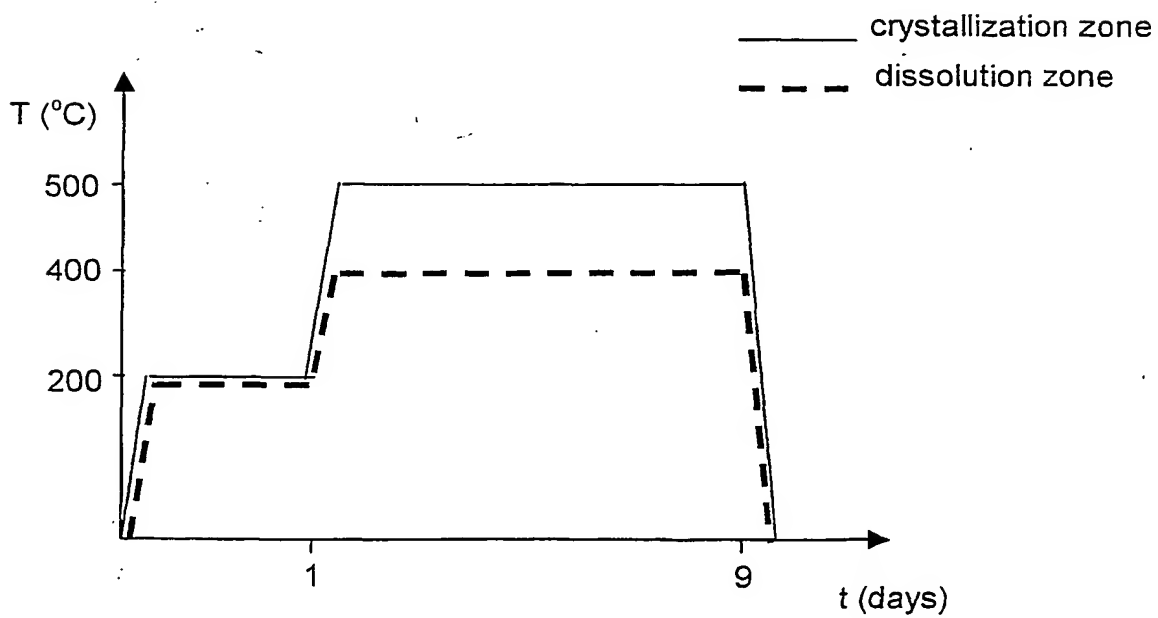


Fig. 14

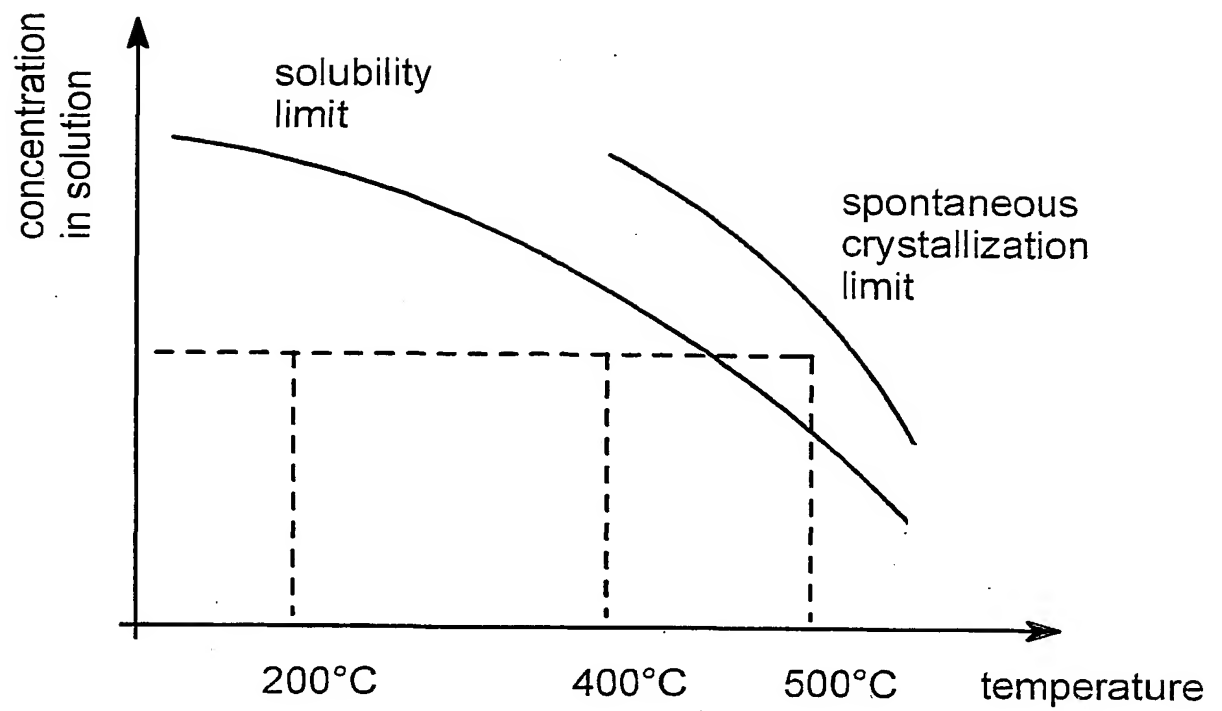


Fig. 15

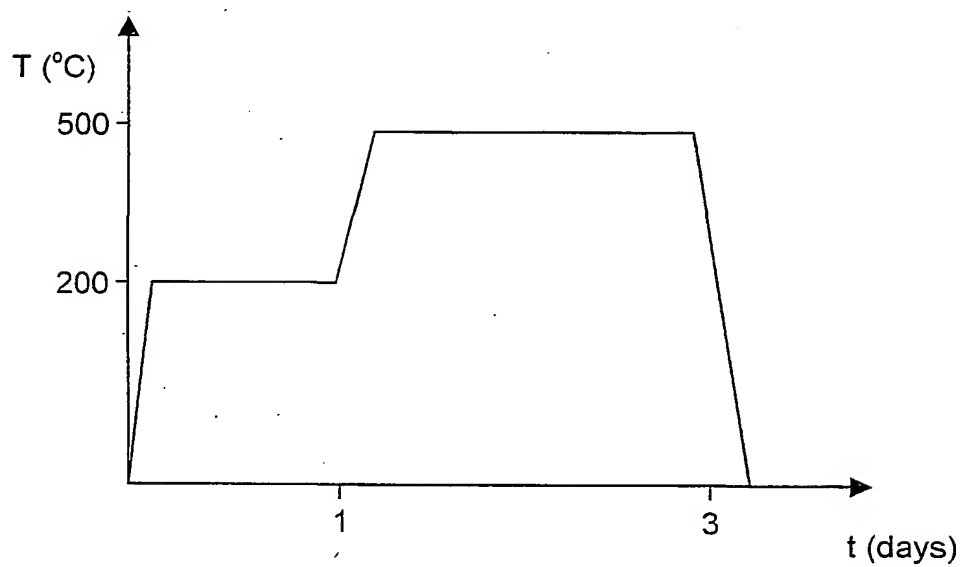


Fig. 16

(19) World Intellectual Property
Organization
International Bureau



(43) International Publication Date
19 December 2002 (19.12.2002)

PCT

(10) International Publication Number
WO 2002/101120 A3

(51) International Patent Classification⁷: **C30B 9/00**,
7/00, 29/40

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(21) International Application Number:
PCT/IB2002/004185

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(22) International Filing Date: 17 May 2002 (17.05.2002)

(81) Designated States (*national*): AE, AG, AL, AM, AT, AU,
AZ, BA, BB, BG, BR, BY, BZ, CA, CH, CN, CO, CR, CU,
CZ, DE, DK, DM, DZ, EC, EE, ES, FI, GB, GD, GE, GH,
GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC,
LK, LR, LS, LT, LU, LV, MA, MD, MG, MK, MN, MW,
MX, MZ, NO, NZ, OM, PH, PL, PT, RO, RU, SD, SE, SG,
SI, SK, SL, TJ, TM, TN, TR, TT, TZ, UA, UG, US, UZ,
VN, YU, ZA, ZM, ZW.

(25) Filing Language: English

(26) Publication Language: English

(30) Priority Data:
P-347918 6 June 2001 (06.06.2001) PL
P-350375 26 October 2001 (26.10.2001) PL

(84) Designated States (*regional*): ARIPO patent (GH, GM,
KE, LS, MW, MZ, SD, SL, SZ, TZ, UG, ZM, ZW),
Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM),
European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR,
GB, GR, IE, IT, LU, MC, NL, PT, SE, TR), OAPI patent
(BF, BJ, CF, CG, CI, CM, GA, GN, GQ, GW, ML, MR,
NE, SN, TD, TG).

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Published:

— with international search report

(88) Date of publication of the international search report:
29 April 2004

*For two-letter codes and other abbreviations, refer to the "Guid-
ance Notes on Codes and Abbreviations" appearing at the begin-
ning of each regular issue of the PCT Gazette.*

(54) Title: PROCESS AND APPARATUS FOR OBTAINING BULK MONOCRYSTALLINE GALLIUM-CONTAINING NITRIDE

(57) Abstract: The present invention refers to an ammonobasic method for preparing a gallium-containing nitride crystal, in which gallium-containing feedstock is crystallized on at least one crystallization seed in the presence of an alkali metal-containing component in a supercritical nitrogen-containing solvent. The method can provide monocrystalline gallium-containing nitride crystals having a very high quality.

WO 2002/101120 A3

INTERNATIONAL SEARCH REPORT

International Application No

PCT/IB 02/04185

A. CLASSIFICATION OF SUBJECT MATTER
IPC 7 C30B9/00 C30B7/00 C30B29/40

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)
IPC 7 C30B

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

PAJ, EPO-Internal

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	FR 2 796 657 A (THOMSON CSF) 26 January 2001 (2001-01-26) the whole document	1-13, 15-26, 30, 37-55, 57-71, 75-79, 81-108
X	US 5 456 204 A (DIMITROV VESSELIN S ET AL) 10 October 1995 (1995-10-10) column 4, line 9 - line 57; figure 1 -/--	50-55, 75-79

☒ Further documents are listed in the continuation of box C.

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Date of the actual completion of the international search

12 February 2003

Date of mailing of the international search report

19/02/2003

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C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT		
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